

**TO MY HUSBAND and MY PARENTS**

**FT-IR SPECTROSCOPIC CHARACTERIZATION of  
the INTERMEDIATES in the SELECTIVE CATALYTIC REDUCTION  
of NO WITH METHANE on Pd/ZrO<sub>2</sub>-WO<sub>x</sub> CATALYST**

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IN PARTIAL FULFILLMENT OF THE REQUIREMENTS  
FOR THE DEGREE  
OF  
MASTER OF SCIENCE**

**By  
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**SEPTEMBER 2004**

I certify that I have read this thesis and in my opinion it is fully adequate, in scope and quality, as a thesis of the degree of Master of Science

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## ABSTRACT

### **FT-IR SPECTROSCOPIC CHARACTERIZATION of the INTERMEDIATES in the SELECTIVE CATALYTIC REDUCTION of NO WITH METHANE on Pd/ZrO<sub>2</sub>-WO<sub>x</sub> CATALYST**

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M.S. in Chemistry

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September 2004

This work involves in situ FT-IR spectroscopic study of the routes of formation, composition and thermal stability of strongly bound NO<sub>x</sub> complexes on the surface of Pd/tungstated zirconia, and transformation of the surface NO<sub>x</sub> complexes in the presence of methane in order to elucidate the mechanism of selective catalytic reduction of NO with methane. Sol-gel polymer-template synthesis was chosen to obtain high surface area in the preparation of the tungstated zirconia used as support (WO<sub>3</sub> nominal content of 18.6 wt %). The Pd(II) ions (0.1 wt%) have been deposited by impregnation. PXRD characterization shows that the support and the catalyst are tetragonal and contain mesoporous phase.

The adsorption of NO at room temperature on the tungstated zirconia shows presence of coordinatively unsaturated Zr(IV) ions. The spectrum of NO adsorbed on palladium modified on tungstated zirconia reveals the existence of two types of Pd(II) sites. No exposed Zr(IV) ions are observed. The surface NO<sub>x</sub> species (N<sub>2</sub>O<sub>3</sub>, nitro and nitrito ions) on both samples are produced at room temperature by oxidation of NO with the W<sup>6+</sup>=O species. In the case of the Pd/tungstated zirconia, palladium(II) can oxidize NO to NO<sub>2</sub> at 623 K.

The adsorption of NO/O<sub>2</sub> mixture at room temperature on the samples studied leads to formation of various kinds of surface nitrates characterized by different modes of coordination. The thermal stability of the nitrate species formed on both samples is comparable: They disappear after dynamic evacuation at 673 K. However, lower concentration of the surface nitrates on the Pd/tungstated zirconia compared to that on the tungstated zirconia indicates that in the former case the nitrates are coordinated to the support.

The experimental results show that methane interacts differently with the NO<sub>x</sub>-precovered tungstated zirconia and Pd/tungstated zirconia although both materials are able to activate methane at the same temperature in absence of adsorbed NO<sub>x</sub> species. In the case of the tungstated zirconia the surface nitrates suppress the oxidation of methane, whereas the NO<sub>x</sub>-precovered Pd/tungstated zirconia catalyzes the formation of nitromethane. The latter compound is considered as a key intermediate in the selective catalytic reduction of NO with methane in excess oxygen. A mechanism, which involves direct activation of methane by the catalyst, leading to the products of the selective reduction (N<sub>2</sub>, CO<sub>2</sub> and H<sub>2</sub>O) is proposed.

**Keywords:** Adsorption of NO and NO/O<sub>2</sub>; In situ FT-IR spectroscopy; tungstated zirconia; Pd supported on tungstated zirconia; NO selective catalytic reduction by methane; Mechanism; Nitromethane.

## ÖZET

### **Pd/ZrO<sub>2</sub>-WO<sub>x</sub> KATALİZÖR ÜZERİNDE METHANE ile SEÇİCİ KATALİTİK İNDİRGENMEDE OLUŞAN ARA ÜRÜNLERİN FT-IR SPEKTROSKOPİK KARAKTERİZASYONU**

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September 2004

Bu çalışma metan ile NO'nun seçici katalitik indirgenme mekanizmasını açıklamak için Pd/tungstenlenmiş zirkonyum yüzeyinde kuvvetlice bağlanmış NO<sub>x</sub> komplekslerinin methane varlığında oluşmasının, kompozisyonun ve termal kararlılığının *in-situ* FT-IR spektroskopik çalışmasını içermektedir. Yüzey alanını geniş elde etmek için tungstenlenmiş zirkonyumun (ağırlıkça 18.6 % WO<sub>3</sub> nominal içerikli) hazırlanmasında Sol-gel polimer-template sentezi seçilmiştir. İmpregnasyon yöntemi kullanılarak Pd(II) iyonları (ağırlıkça 0.1%) depolanmıştır. PXRD karakterizasyonu katalizörün tetragonal ve mesoporus fazlarını içerdiğini göstermiştir.

Tungstenlenmiş zirkonyum üzerine oda sıcaklığında NO adsorpsiyonu koordinasyona açık Zr<sup>4+</sup> iyonlarının olduğunu göstermiştir. Pd içeren numunenin NO adsorpsiyonu iki çeşit Pd(II)'nin bulunduğunu açığa çıkarmış ve koordinasyona açık Zr<sup>4+</sup> iyonları gözlenmemiştir. İki numune üzerindeki NO<sub>x</sub> türleri (N<sub>2</sub>O<sub>3</sub>, nitro and nitrito iyonları) oda sıcaklığında NO'nun W<sup>6+</sup>=O gruplarıyla oksitlenmesi sonucu üretilmiştir. Pd/tungstenlenmiş zirkonyum üzerinde paladyum(II) 623 K de NO'yu NO<sub>2</sub>'ye oksitleyebilmektedir.

NO ve O<sub>2</sub> karışımının oda sıcaklığında, çalışılan numunelere adsorpsiyonu, koordinasyonları farklı olan çeşitli yüzey nitratlarının oluşmasını

sağlamıştır. Her iki numunede de oluşan nitratların termal kararlılıkları benzerdir. 673 K deki dinamik vakumlama sonrasında nitratlar yok olmuşlardır. Bununla beraber Pd/tungstenlenmiş zirkonyum üzerinde oluşan yüzey nitratlarının düşük konsantrasyonu, nitratların tungstenlenmiş zirkonyuma koordinasyonunu belirtmektedir.

Adsorbe olmuş  $\text{NO}_x$  türlerinin yokluğunda iki numune de hidrokarbonu aynı sıcaklıkta aktifleştirmiş olmasına rağmen, deneysel sonuçlar metanın  $\text{NO}_x$  ile daha önce kaplanmış tungstenlenmiş zirkonyum ve Pd/tungstenlenmiş zirkonyumun farklı şekillerde etkileştiğini göstermiştir. Tungstenmiş zirkonyumda yüzey nitratları metanın oksidasyonunu bastırırken,  $\text{NO}_x$  ile daha önce kaplanmış Pd/tungstenlenmiş zirkonyum nitrometan oluşmasını katalizlemektedir. Nitrometan,  $\text{NO}$ 'nun metan ile seçici katalitik indirgenmesinde anahtar ara ürün olarak düşünülmektedir. Hidrokarbonun direk aktivasyonunu içeren ve seçici indirgenme ürünlerini ( $\text{N}_2$ ,  $\text{CO}_2$  and  $\text{H}_2\text{O}$ ) oluşturan bir mekanizma önerilmiştir.

**Anahtar Kelimeler:**  $\text{NO}$  and  $\text{NO}/\text{O}_2$  adsorpsiyonu; *in-situ* FT-IR spektroskopisi; tungstenlenmiş zirkonyum; Pd depolanmış tungstenlenmiş zirkonyum;  $\text{NO}$ 'nu metan ile seçici katalitik indirgenmesi; Mekanizma; Nitrometan.



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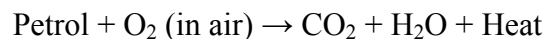


# 1. INTRODUCTION

## 1.1. General about the Selective Catalytic Reduction of NO<sub>x</sub>

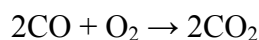
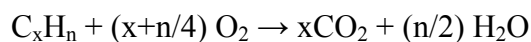
Fossil fuels are combusted in transport devices, power plants, house heating and the chemical industry. Since the concept is almost the same for each application, transport devices are exemplified in order to explain how undesirable gases are produced.

Power is supplied to the majority of automobiles and trucks by a spark ignited gasoline engine. Gasoline is a mixture of paraffins and aromatic hydrocarbons, which combust in air very efficiently. In the engine the following ideal combustion reaction is considered to take place:

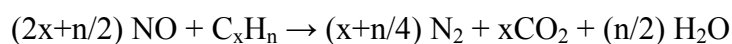
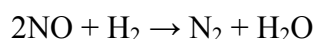
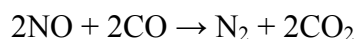


In addition to these products, carbon monoxide (CO), unburned hydrocarbons (HC), nitrogen oxides (NO<sub>x</sub>), hydrogen (H<sub>2</sub>) and oxygen (O<sub>2</sub>) can be identified in exhaust gases [1]. NO<sub>x</sub>, CO and HC are the primary atmospheric pollutants. CO poisons human-beings. HC is a potential greenhouse gas. Reaction between HC and NO<sub>x</sub>, which is enhanced by sunlight, leads to the formation of ground level ozone. NO<sub>x</sub> particularly has the ability to cause the formation of photochemical smog, acid rain and airborne particulate, through ammonium nitrate formation [1,2,3].

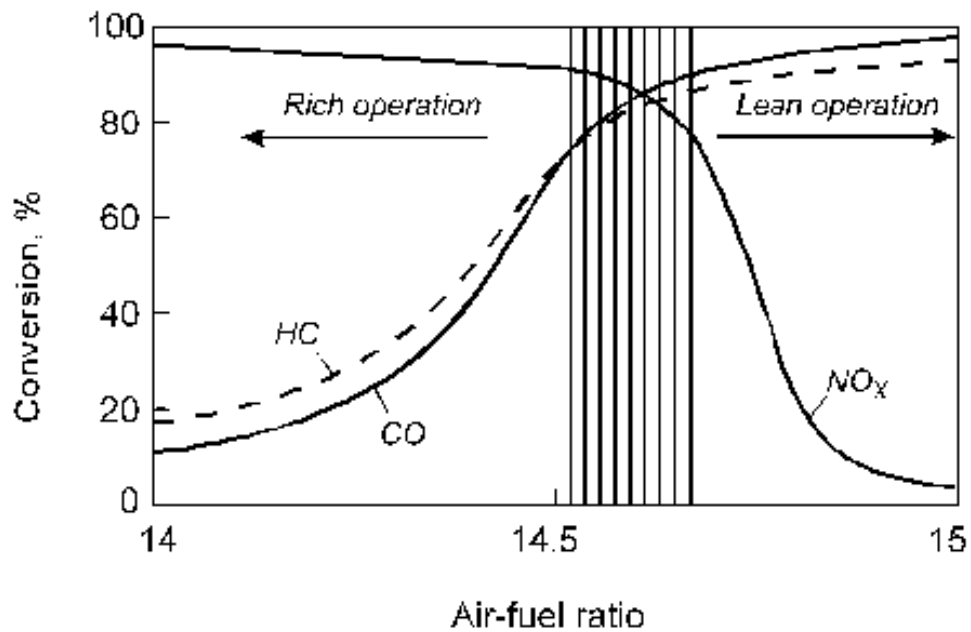
Because of the environmental reasons, in automobile exhaust gases CO and HC should be oxidized to CO<sub>2</sub> and H<sub>2</sub>O meanwhile NO<sub>x</sub> should be reduced to the desired product N<sub>2</sub>. The oxidation reactions are:



And the reduction reactions are:

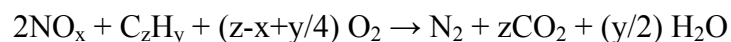


New automobile technology requires catalysts, which cause above reactions to occur at lower temperatures. Since the catalyst simultaneously promotes these reactions, it is called *the three-way catalyst (TWC)*. The catalytic performance of the three-way catalyst is a function of the engine air to fuel ratio (Fig.1). The best performance of TWC is obtained at the air-fuel ratio of 14.6:1. So non-selective reduction of NO<sub>x</sub> is accomplished by HC, CO and/or H<sub>2</sub>. Thus, the primary pollutants in the exhaust gases are converted to desired chemical products [1,2,3].



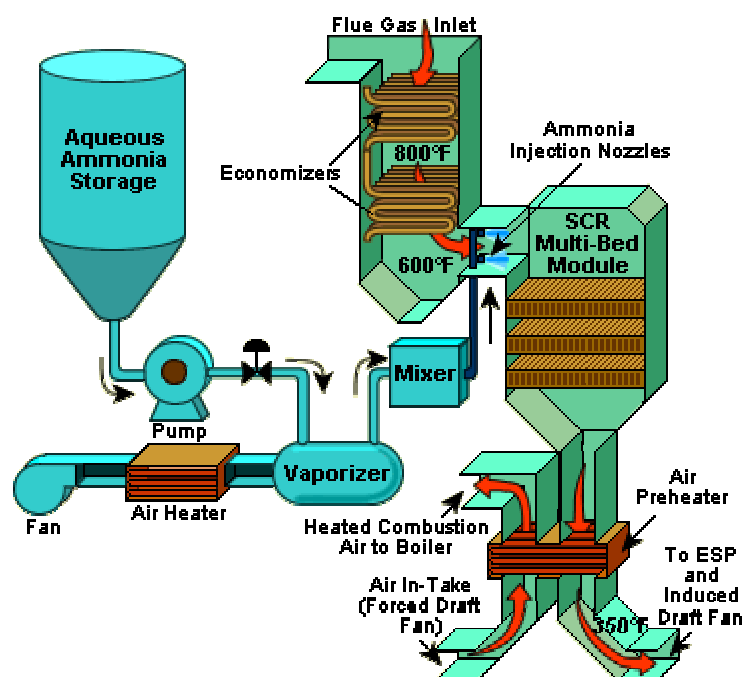
**Figure 1.** The conversion efficiency (%) of a three-way catalyst as a function of A/F-ratio. The lambda window, an A/F-ratio of 14.6 corresponds to stoichiometric operation,  $\lambda = 1$  [4].

The TWC is inefficient to reduce NO<sub>x</sub> for the lean-burn engine applications ( $\lambda > 1$ ), e.g. diesel engines and lean burn gasoline engines. The NO<sub>x</sub> reduction by HC under the excess oxygen condition is called *selective catalytic reduction (SCR)*, in which the reductant intentionally reacts with nitrogen oxides instead of being burned by oxygen [1,5,6]:



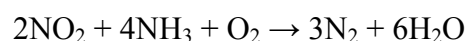
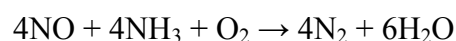
## 1.2. Selective Catalytic Reduction by Methane – What is the advantage?

Industrial sources of NO<sub>x</sub> are from stationary plants, which are coal- and oil-fired power plants, incinerators and gas turbines. NO<sub>x</sub> is currently removed from exhaust streams in lean burn conditions and at lower temperature by the selective catalytic reduction with ammonia. A conventional SCR system is shown in Fig. 2 [7].



**Figure 2.** Example SCR System for NO<sub>x</sub> control in a boiler.

In SCR systems, ammonia vapor is used as the reducing agent and is injected into the flue gas stream, passing over a catalyst. The SCR with ammonia breaks down nitrogen oxide to form molecular nitrogen and water with the following reactions [8];

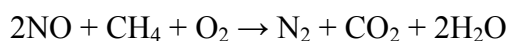


NO<sub>x</sub> emission reductions over 80-90% can be achieved and the optimum temperature is usually between 300°C and 400°C, which is normally the flue gas temperature at the economizer outlet. The V<sub>2</sub>O<sub>5</sub> loaded on TiO<sub>2</sub>, which is

further doped by manganese or molybdenum oxides, is the most used catalyst in the coal-fired plants. Yet there are other catalysts used industrially, which are activated carbon or platinum.

Even though SCR by  $\text{NH}_3$  is a very promising technology in terms of efficiency and sulfur tolerance, it has some drawbacks at the same time. The toxicity is the main drawback in the use of ammonia and then precautions have to be taken during storage and transportation. The SCR with  $\text{NH}_3$  produces relatively high  $\text{N}_2\text{O}$  emissions compared to a conventional diesel engine. The amount of ammonia injected into the SCR is critical to its successful operation. If too little ammonia is injected, some of the  $\text{NO}_x$  will not be converted and if too much ammonia is injected, some of the ammonia will "slip" past the catalyst and become a new emission problem. So the ammonia slip in SCR processes should be minimized that supposes an optimization of the ammonia feed. Finally, accumulation of ammonium sulfates can induce significant pressure drops and/or further corrosion phenomena, which alter the efficiency of SCR processes. Therefore this SCR with  $\text{NH}_3$  requires high capital investment, infrastructure development and operational cost [3,5].

Presently, the use of hydrogen or hydrocarbon, mainly methane, could be an alternative, which offers new perspective in the utilization of natural gas. Selective catalytic reduction with hydrocarbons (SCR-HC) is expected to be a more convenient and cheaper alternative. In this respect, particularly the use of methane, readily available as natural gas, already in use as fuel and not corrosive, is very attractive. It also removes the storage problem. Furthermore, the slippage of hydrocarbon is more environmentally benign than ammonia, although it is still necessary to minimize the slippage. Thus, the use of methane offers the opportunity for significantly reduced capital and operating costs [10]. The selective catalytic reduction of  $\text{NO}_x$  with methane is according to the following reaction:



The most possible applications of this technology using methane as a reducing agent are for exhaust from natural gas-fired power plants and lean-burn natural-gas engines. The catalyst for mobile applications should have high activity and exceptional durability. The catalyst, which is candidate for the industrial power plants, should not be poisoned from water vapor and  $\text{SO}_2$ .

Zeolite-based catalysts (e.g. Co-, Ga-, In-ZSM-5) can be particularly effective [3,11-16]. However, their NO<sub>x</sub> reduction activity and durability is deteriorated when exposed to wet reaction conditions [3,12,14,16]. Use of simple oxide support with strong surface acidity provides an alternative approach to achieve better performance of the catalysts for the selective catalytic reduction of NO with methane in moist streams. The most promising materials as catalysts are supported metal oxides (e.g. Pd/TiO<sub>2</sub>, Pt/Al<sub>2</sub>O<sub>3</sub>, Pd/WO<sub>x</sub>-ZrO<sub>2</sub>,...) [17-19]. They exhibit activity comparable to the zeolitic catalyst in the SCR of NO<sub>x</sub> by CH<sub>4</sub>. Unlike zeolitic catalysts, supported noble metal oxides are much more stable hydrothermally. Furthermore, flexibility in the preparation of mixed metal oxides with a desired composition puts importance for practical catalysts [20].

### **1.3. Main Characteristics of Tungstated Zirconia as a Support**

Acidity is the important phenomenon in oxide supports for the selective catalytic reduction of NO<sub>x</sub> with methane since the acidity of the support determines the activity toward CH<sub>4</sub> in the absence of zeolitic structure [20,21]. Acidity of the supports can be modified by choosing the appropriate synthesis techniques, doping with transition and/or non-transition oxides and adjusting the amount of modifiers.

Zirconia has taken interest as a support [18,22-26] due to the amphoteric properties [27]. Stable monoclinic and metastable tetragonal phases can be intentionally obtained by using various preparation routes, which have different starting raw materials and different pretreatment conditions, and by adding tiny amount of impurities [28-34]. Zhao et al. [35] reported that tetragonal zirconia has only Lewis acid sites on the surface but monoclinic zirconia has both Brønsted and Lewis acid sites. Bolis et al. [36] stated that Lewis acidic sites on the surfaces of tetragonal zirconia are much stronger than those on the surfaces of monoclinic zirconia even though the Lewis acid sites are more abundant on monoclinic zirconia. The acidity of the zirconia can be changed by doping with sulfate ions and tungsten oxide, both of which enhance the acidity. Whereas sulfated zirconia shows more acidic character than tungstated zirconia [36-38], sulfated zirconia suffers from rapid deactivation, sulfur loss during reaction

conditions and regeneration. Thus, tungstated zirconia has taken more attention as a strong solid acid.

It has been reported that  $\text{WO}_3$  supported on  $\text{ZrO}_2$  exhibits strong Brønsted and Lewis acidity when  $\text{WO}_3$  covered the  $\text{ZrO}_2$  surface as a monolayer [39-42]. Additionally, the preparation method involving simultaneous coprecipitation of tungsten with the formation of hydrous zirconia results in a catalyst and/or a support with increased strong acid site density as compared to the catalyst and/or the support prepared by tungsten impregnation of hydrous and calcined zirconia [43-46]. Chin et al. [18] observed that tungstated zirconia as a support of a  $\text{DeNO}_x$  catalyst is more tolerant to water vapor because of the simple structure and shows resistance to  $\text{SO}_2$  poisoning.

In order to increase the activity and selectivity toward the reduction of NO with methane Pd is deposited on the tungstated zirconia [18,19,47].

#### **1.4. Mechanism of Selective Catalytic Reduction of $\text{NO}_x$ on Pd-containing Catalysts**

Lobree et al. [48] proposed a reaction mechanism for the reduction of NO with  $\text{CH}_4$  by using mass spectroscopy and in-situ infrared spectroscopy. They observed that the reduction of NO by  $\text{CH}_4$  started by the interaction of methane with the adsorbed NO above 650 K, which produces  $\text{CH}_2\text{NO}$  (or its isomer  $\text{CHNOH}$ ) in the form of  $\text{Z}^-\text{H}^+[\text{Pd}(\text{H})(\text{CH}_2\text{NO})]^+\text{Z}^-$  species.  $\text{CH}_2\text{NO}$  decomposes to produce water and highly reactive neutral CN species ( $\text{Z}^-\text{H}^+[\text{Pd}(\text{H})(\text{CN})]^+\text{Z}^-$ ) as intermediates, which further react with NO or  $\text{O}_2$  (if present). Reaction with NO forms  $\text{N}_2$  and CO, whereas reaction with  $\text{O}_2$  yields NO and CO. For this process the principal active component in Pd-H-ZSM-5 is found to be  $\text{Pd}^{2+}$ .

Shimizu et al. [49] investigated the mechanism of NO reduction by methane in the presence of  $\text{O}_2$  over Pd-H-Mordenite. They concluded from in-situ UV-Vis, in-situ IR data and kinetic results that  $\text{CH}_4$ -derived reactive species reduces the adsorbed NO on  $\text{Pd}^{2+}$  in order to produce  $\text{NH}_4^+$  on the zeolite acid sites. The formed  $\text{NH}_4^+$  reacts with  $\text{Pd}^{2+}$ -nitrosyl and  $\text{NO}_2$  species, which results in the desired product  $\text{N}_2$ . They also believe that  $\text{Pd}^{2+}$ -NO and  $\text{NH}_4^+$  are the possible key intermediates for this reaction mechanism and isolated  $\text{Pd}^{2+}$  ions and

Brønsted acid sites are indispensable for intermediates. And the kinetic results confirm the proposed mechanism.

Lukyanov et al. [50] stated from kinetic studies that interaction of methane with adsorbed  $\text{NO}_2$  initiated the catalytic reduction of  $\text{NO}_x$  into  $\text{N}_2$  and oxidation of  $\text{CH}_4$ . The intermediate species,  $\text{CH}_3\bullet$ , was formed due to H abstraction of  $\text{NO}_2$  since  $\text{NO}_2$  is a free radical and stronger oxidizing agent than  $\text{NO}$ .

Mechanistic study on titania-supported palladium pointed out  $\text{NH}_3$  as an intermediate [17,51]. Ozkan et al. observed that the linearly adsorbed  $\text{NO}$  on metallic Pd disappeared upon methane addition and  $\text{NH}_3$  adsorbed on Lewis acid sites has been formed. They proposed that methane was activated on  $\text{Pd}^0$  sites.

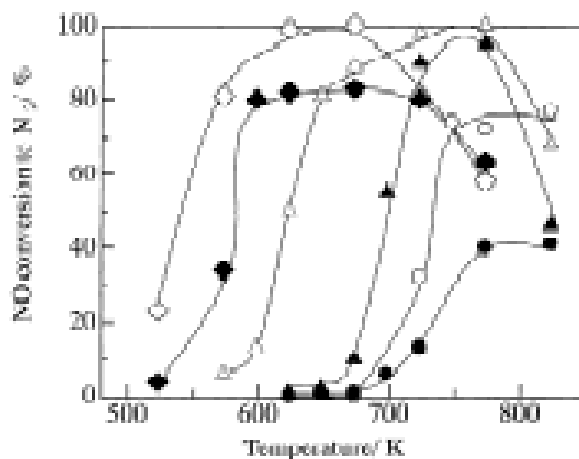
Sun et al. [52] suggested nitromethane as an intermediate in the reduction of  $\text{NO}$  over  $\text{Co}^{2+}$  modified ZSM-5 catalysts. In the oxidizing atmosphere  $\text{NO}$  easily interacts with Co-ZSM-5, resulting in the formation of adsorbed  $\text{NO}_2$  species. And methane reacts with adsorbed  $\text{NO}_2$  to produce nitromethane intermediate, which further reacts with  $\text{NO}_2$  to yield  $\text{N}_2$ ,  $\text{H}_2\text{O}$  and  $\text{CO}_2$ .

If nitromethane is observed as an intermediate in the selective catalytic reduction of  $\text{NO}$  with  $\text{CH}_4$ , isocyanide ( $\text{NCO}$ ), hydrogen cyanide ( $\text{HCN}$ ), ammonia ( $\text{NH}_3$ ), carbamic acid, nitrous oxide ( $\text{N}_2\text{O}$ ), cyanuric acid ( $\text{HNCO}$ ), melamine can be detected as decomposition products/intermediates [53-57].

The temperature dependence of  $\text{NO}$  conversion to nitrogen with various hydrocarbons in excess oxygen (Fig. 3) displays a volcano shape [58]. This indicates that strongly bound  $\text{NO}_x$  surface complexes are involved in the selective conversion of  $\text{NO}$  to molecular nitrogen in excess oxygen.

The aims of this study are:

- (i) to determine by means of in situ FT-IR spectroscopy routes of formation, composition and thermal stability of strongly bound  $\text{NO}_x$  complexes on the surface of Pd/tungstated zirconia, and
- (ii) to investigate transformation of surface  $\text{NO}_x$  complexes in the presence of methane in order to elucidate the reaction mechanism.



**Figure 3.** NO conversion to nitrogen on Ag/Al<sub>2</sub>O<sub>3</sub> using various n-alkanes: (●) methane, (○) ethane, (▲) propane, (△) butane, (◇) hexane, (★) octane. Conditions: NO = 1000 ppm, alkane = 6000 ppm, O<sub>2</sub> = 10 %, H<sub>2</sub>O = 2 %, and W/F = 0.12 g.s/cm<sup>3</sup>, except for methane-SCR (W/F = 0.9 gs/cm<sup>3</sup>) [58]

### 1.5. Identification of adsorbed NO<sub>x</sub> species by FT-IR Spectroscopy

Adsorptions of NO and its coadsorption with O<sub>2</sub> lead to formation adsorbed NO<sub>x</sub> species, whose identifications are important for the mechanistic study of selective catalytic reduction of NO.

The negatively charged species usually observed on the surface of the catalysts are nitrite (NO<sub>2</sub><sup>-</sup>) and nitrate (NO<sub>3</sub><sup>-</sup>) anions. The free nitrite anion has a C<sub>s</sub> symmetry and absorption bands due to ν<sub>as</sub>(NO<sub>2</sub>) and ν<sub>s</sub>(NO<sub>2</sub>) modes are at 1330 and 1260 cm<sup>-1</sup>, respectively [59]. When NO<sub>2</sub><sup>-</sup> is coordinated by one or two of its oxygen atoms, nitrito species are formed. When NO<sub>2</sub><sup>-</sup> is coordinated by its nitrogen atom, nitro compounds are formed. Characteristic IR regions for nitro/nitrito compounds are given in Table 1.

The free nitrate is planar and has a D<sub>3h</sub> symmetry. It shows three IR active modes: asymmetric stretching (ν<sub>3</sub>) at 1430 cm<sup>-1</sup>, out-of-bending (ν<sub>2</sub>) at 825 cm<sup>-1</sup> and in-plane-bending (ν<sub>4</sub>) at 722 cm<sup>-1</sup> [60]. ν<sub>1</sub> is symmetric and is only observed in Raman spectra. After coordination, ν<sub>1</sub> becomes IR active and the degeneracy of ν<sub>3</sub> is removed so that ν<sub>3</sub> splits into two components. The magnitude



of the splitting depends on the coordination type of the nitrates. The absorption ranges for nitrates are presented in Table 1.

The IR absorption bands for nitrite and nitrates sometimes overlap in the 1350-1550  $\text{cm}^{-1}$  region. In that case, combination bands of nitrates can be used for structural identification. The combination bands of the bridged nitrates are at 2845-2800  $\text{cm}^{-1}$  [ $\nu_s(\text{N}=\text{O}) + \nu_s(\text{NO}_2)$ ] and pair bands at 1980-1960 [ $\nu_s(\text{NO}_2) + \delta(\text{ONO})$ ] and 1900-1890  $\text{cm}^{-1}$  [ $\nu_s(\text{NO}_2) + \delta(\text{ONO})$ ]. Bidentate nitrates produce combination bands in the region of 2600  $\text{cm}^{-1}$  [ $\nu_s(\text{N}=\text{O}) + \nu_s(\text{NO}_2)$ ] and pair of bands at 1755 and 1700  $\text{cm}^{-1}$  [ $\nu_s(\text{NO}_2) + \delta(\text{ONO})$ ] [60].

Stability of adsorbed  $\text{NO}_x$  species can give information about their nature. The noncharged species, e.g.  $\text{NO}$ ,  $(\text{NO})_2$ ,  $\text{NO}_2$ ,  $\text{N}_2\text{O}_3$  and  $\text{N}_2\text{O}_4$ , are generally weakly adsorbed and easily removed from the surface upon evacuation at room temperature. But charged species, e.g.  $\text{NO}^+$ ,  $\text{NO}_2^-$ ,  $\text{NO}_3^-$ ,  $\text{NO}^-$  are stable. They need to be heated at elevated temperatures in order to desorb from the surface. The nitro species are more stable than the nitrito species and bridged and bidentate nitrates are more thermally stable than the monodentate nitrates.

**Table 1:** Spectral characteristics of NO<sub>x</sub> species observed on the metal oxides  
[59,60,62,63]

NO <sub>x</sub> Species	Vibration Modes	Wavenumbers (cm <sup>-1</sup> )
Free nitrite ion, NO <sub>2</sub> <sup>-</sup>	$\nu_{as}(\text{NO}_2)$	1250
	$\nu_s(\text{NO}_2)$	1335
	$\delta(\text{ONO})$	830
Nitro, M-NO <sub>2</sub>	$\nu_{as}(\text{NO}_2)$	1370-1470
	$\nu_s(\text{NO}_2)$	1320-1340
	$\delta(\text{ONO})$	820-850
Nitrito, M-O-NO	$\nu(\text{N=O})$	1400-1485
	$\nu(\text{NO})$	1050-1100
	$\delta(\text{ONO})$	820-840
Chelated Nitrito, (M-O <sub>2</sub> )=N	$\nu_{as}(\text{NO}_2)$	1270-1390
	$\nu_s(\text{NO}_2)$	1170-1225
	$\delta(\text{ONO})$	840-860
Bridging nitro, M-O-N(O)-M	$\nu_{as}(\text{NO}_2)$	1390-1520
	$\nu_s(\text{NO}_2)$	1180-1260
Bidentate nitro	$\nu_{as}(\text{NO}_2)$	1390-1520
	$\nu_s(\text{NO}_2)$	1180-1260
Free nitrate ion, NO <sub>3</sub>	$\nu_{as}(\text{NO}_2)$	1430
Monodentate nitrate, M-O-NO <sub>2</sub>	$\nu_{as}(\text{NO}_2)$	1450-1570
	$\nu_s(\text{NO}_2)$	1250-1330
	$\nu(\text{NO})$	970-1035
Bidentate nitrate, M-O <sub>2</sub> NO	$\nu_{as}(\text{NO}_2)$	1200-1310
	$\nu_s(\text{NO}_2)$	1003-1040
	$\nu(\text{NO})$	1500-1620
Bridged nitrate, (M-O) <sub>2</sub> =NO	$\nu_{as}(\text{NO}_2)$	1200-1260
	$\nu_s(\text{NO}_2)$	1000-1030
	$\nu(\text{NO})$	1590-1660

## 2. EXPERIMENTAL

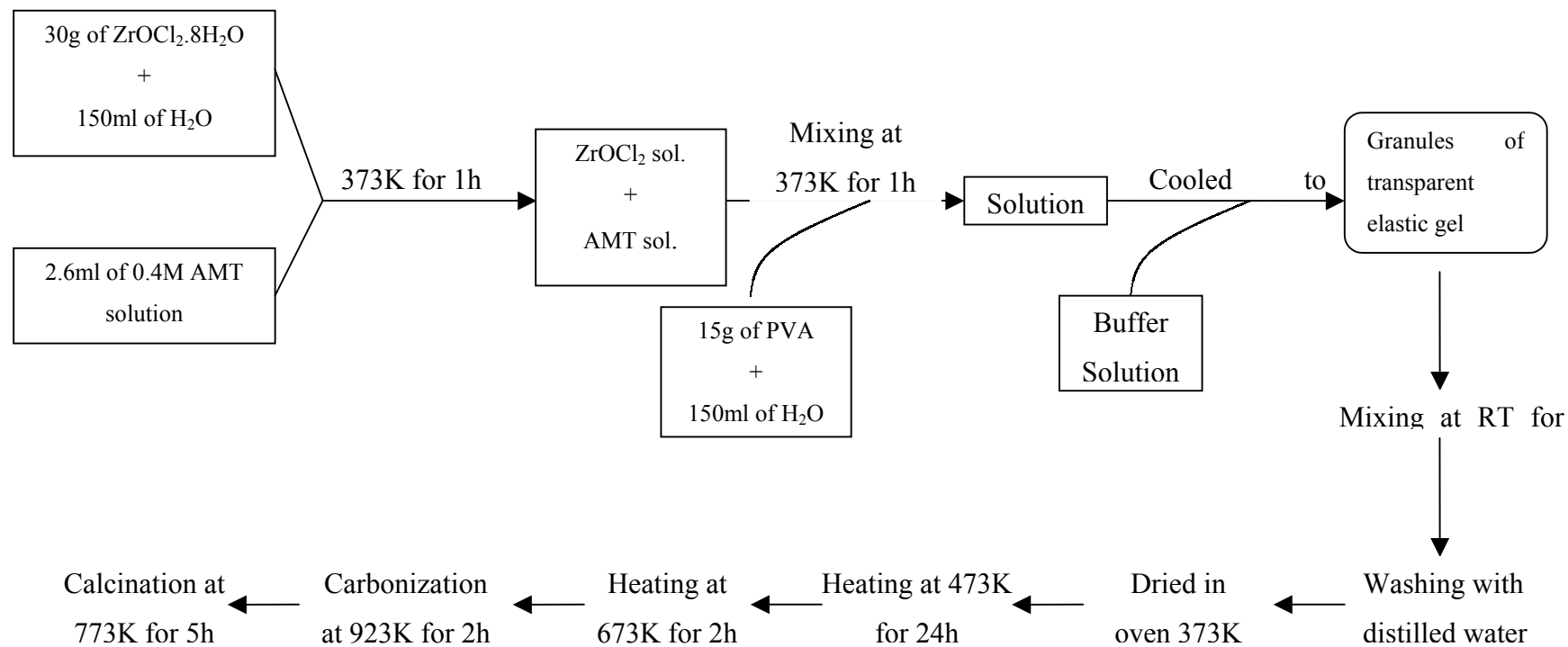
### 2.1. Sample Preparation

#### 2.1.1. Tungstated zirconia

The mesoporous tungstated zirconia was synthesized by using polyvinyl alcohol (PVA) as a template [34]. The following procedure was applied; 30 g of  $ZrOCl_2 \cdot 8H_2O$  was dissolved in 150 ml of  $H_2O$ . 2.6 ml of 0.4 M ammonium metatungstate solution was added to zirconium oxychloride solution while stirring. The mixed solution was heated up to  $100^\circ C$  in a water bath and kept for 1 h at this temperature. Besides, the aqueous solution of PVA was prepared by dissolving 15 g of PVA in 150 ml of  $H_2O$  (on heating). The hot solutions of PVA and zirconium tungstate were mixed and kept for 1 h at  $100^\circ C$ , then cooled to  $60^\circ C$ . The colloidal solution was poured into a prepared buffer solution ( $NH_4Cl + NH_4OH$ ) under stirring. Granules of a transparent elastic gel were formed. And the obtained mixture stayed for 1 h at room temperature while stirring. Then it was washed with distilled water several times until the disappearance of chlorine anions in the washing water. The washed gel was dried in a drying oven at 373 K whereupon the transparent gel was heated up to 473 K and kept at this temperature for 24 h in air. Then the sample was placed into a quartz tube and heated slowly under vacuum up to 673 K. It stayed for 2 h at this temperature. Afterwards, the sample was heated up to the final carbonization temperature of 923 K and let to stand for 2h at this temperature. The obtained sample was calcined for 5 h at 773 K in air to burn the carbon-containing compounds. The black carbonized sample was completely white after ~30 minute (see flow chart 1).

The finally obtained tungstated zirconia sample was heat treated initially at 873 K then at 973 K for 1 h in order to follow the behavior of mesoporous phase. The nominal content of  $WO_3$  is 18.6 wt %.

**Flow Chart 1 for the preparation of the WZ:**



This method is preferred to prepare the tungstated zirconia sample because:

- Simultaneous coprecipitation of tungsten with the formation of hydrous zirconia produces a material with increased strong acid site density,
- High surface area can be obtained due to the presence of the mesoporous phase,
- $\text{WO}_3$  can cover the  $\text{ZrO}_2$  surface as a monolayer,
- Growing of  $\text{ZrO}_2$  crystals can be retarded due to pinning effect of  $\text{WO}_3$  and mesoporous phases.

In this synthesizing method, PVA acts as a templating agent in the coprecipitation of tungsten and hydrous zirconia and can remain in the material up to temperatures of 600-700°C. So the crystallization of the zirconia occurs without a collapse of the mesoporous structure during the carbonization step. The residue of PVA after carbonization can be removed easily in the oxidizing atmosphere at lower temperature (500°C).

The tungstated zirconia notations used further in the text are summarized in Table 2.

**Table 2:** Tungstated zirconia sample notations

Sample	Treatment
WZ200	After drying the precipitate at 200 <sup>0</sup> C for 24 h in air
WZ400	After heating in vacuum at 400 <sup>0</sup> C for 2 h
WZ650	After heating in vacuum at 650 <sup>0</sup> C for 2 h
WZ	After calcination at 500 <sup>0</sup> C for 5 h
WZ600HT	After heating at 600 <sup>0</sup> C for 1 h
WZ700HT	After heating at 700 <sup>0</sup> C for 1 h

### 2. 1. 2. Zirconia

The mesoporous zirconia was synthesized just like in the case of the mesoporous tungstated zirconia but without using tungstate and the final carbonization temperature was chosen as 873 K.

The pure zirconia notations used further in the text are summarized in Table 3.

**Table 3:** Pure zirconia sample notations

Sample	Treatment
Z200	After drying the precipitate at 200 <sup>0</sup> C for 24 h in air
Z400	After heating in vacuum at 400 <sup>0</sup> C for 2 h
Z600	After heating in vacuum at 600 <sup>0</sup> C for 2 h
Z	After calcination at 500 <sup>0</sup> C for 5 h

### 2. 1. 3. Palladium Modified Tungstated Zirconia

Palladium nitrate is used as a source of Pd<sup>2+</sup> ions. 0.001 M Pd<sup>2+</sup> solution was prepared for the synthesis of 0.10% Pd on tungstated zirconia. 1.5 g of WZ was impregnated with 14.1 ml of 0.001 M Pd<sup>2+</sup> solution. The impregnated samples were dried by stirring at mild heating. Then it was calcined at 773 K for 5 hours.

Pd/WZ notation for palladium modified tungstated zirconia is used further in the text.

### 2. 2. Surface Area Measurements and XRD

The BET surface area of the samples was measured by nitrogen adsorption at 77 K by using a MONOSORP apparatus from Quantachrome. Before the measurements, the samples were dehydrated at 573 K for 1 hour.

XRD analysis was performed on a Rigaku Miniflex diffractometer with Ni-filtered Cu K<sub>α</sub> radiation at ambient conditions. The scan speed was 1°/min.

### 2. 3. IR Spectroscopy

The FT-IR spectra were recorded on a Bomem MB 102 FT-IR (Hartman & Braun) spectrometer equipped with a liquid-nitrogen cooled MCT detector at resolution of 4 cm<sup>-1</sup> (128 scans).

### **2. 3. 1. Experimental Setup**

Two different types of IR cell were used in the experiments. One of the IR cell equipped with NaCl windows allowed the activation of the sample at high temperatures and the recording of the spectra at ambient temperature. The other type of the IR cell (Xenonum Scientific SVCS, USA) allowed recording of the spectra at ambient and elevated temperatures (with BaF<sub>2</sub> windows). The sample holder of the cell can be moved up and down relatively to the light beam, which gives the possibility for the subtraction of the gas phase spectrum when needed. . The IR cell is connected to a vacuum/adsorption apparatus.

### **2. 3. 2. Activation of the Samples**

Self-supporting discs (0.040 g/cm<sup>2</sup>) were used for the FT-IR studies. The pressed Pd/WZ sample was activated by heating for 1 h in vacuum at 723 K and in oxygen (13.3 kPa) at the same temperature followed by evacuation for 1 h at that temperature. The pressed WZ sample was activated by heating for 1 h in vacuum at 723 K and in oxygen (13.3 kPa) at the same temperature followed by evacuation for 1 h at 573 K.

The spectra of the activated sample were taken at high temperature and room temperature, which were used as background references. The spectra of the samples that were subjected to heat treatments at elevated temperatures were recorded at those temperatures. The high temperature background reference was used in the subtraction of the spectra taken at high temperatures and correspondingly the room temperature background reference was used for the spectra registered below 423 K.

When the experiment were performed at high temperatures, changes in the OH region could not detected because the water vapor (if produced) adsorbed dissociatively on the BaF<sub>2</sub> windows, which were cooled by running water.

### **2. 3. 3. Adsorption of NO and NO/O<sub>2</sub>**

99.9 % (Air products) purity of NO was used. NO adsorption was conducted at room temperature with the introduction of 1.33 kPa of NO and the evolutions of the IR spectra with time were taken.

Co-adsorption of NO and O<sub>2</sub> was accomplished at room temperature with the introduction of gas mixture (1:2) of NO and O<sub>2</sub> for a given period of time.

The thermal stability of the created NO<sub>x</sub> species was tested by heating the catalyst for 15 or 20 min under vacuum in the temperature range 473-723 K.

### **2. 3. 4. Interaction of the CH<sub>4</sub> with the Catalysts**

8 kPa of methane was added into the IR cell in order to observe the interaction of CH<sub>4</sub> with the catalyst. Then, the closed cell was heated from 523K to 723 K and the samples were allowed to stay for 20 min at each temperature level.

### **2. 3. 5. Interaction of the Methane with the NO<sub>x</sub>-precovered catalysts**

After the formation of NO<sub>x</sub> species by room temperature adsorption of NO and O<sub>2</sub> (1:2) followed by evacuation for 15 min, 7.33 kPa of CH<sub>4</sub> was added. The interaction of the methane with the NO<sub>x</sub>-precovered catalyst was observed in the temperature range 523 – 723 K. The interaction time was chosen 15 or 20 min for each temperature level.



### 3. RESULTS AND DISCUSSION

#### 3. 1. Characterization of the Samples

##### 3. 1. 1. BET Surface Area Measurements and XRD

**Table 4:** BET surface areas of the samples

Sample	BET surface area [m <sup>2</sup> /g]
ZrO <sub>2</sub>	153
WZ	210

##### 3. 1. 1. 1. Tungstated zirconia

X-ray diffraction pattern of the heated sample at 673 K, denoted by WZ 400, shows one sharp peak at 2.9° and two broad features in the range of 2θ from 20 to 38° and from 40 to 70° (Fig. 4). The broad peaks indicate a very low degree of crystallinity. Existence of mesoporous phase in the sample can be determined from the sharp peak at low angle [64].

The diffractogram of the carbonized sample at 923 K, designated by WZ 650, reveals that it consists of crystalline tetragonal zirconia phase and randomly distributed mesoporous phase.

The size of crystallites was calculated by the use of the Scherrer's equation [65]:

$$t = 0.9\lambda / (B \cdot \cos\theta_B)$$

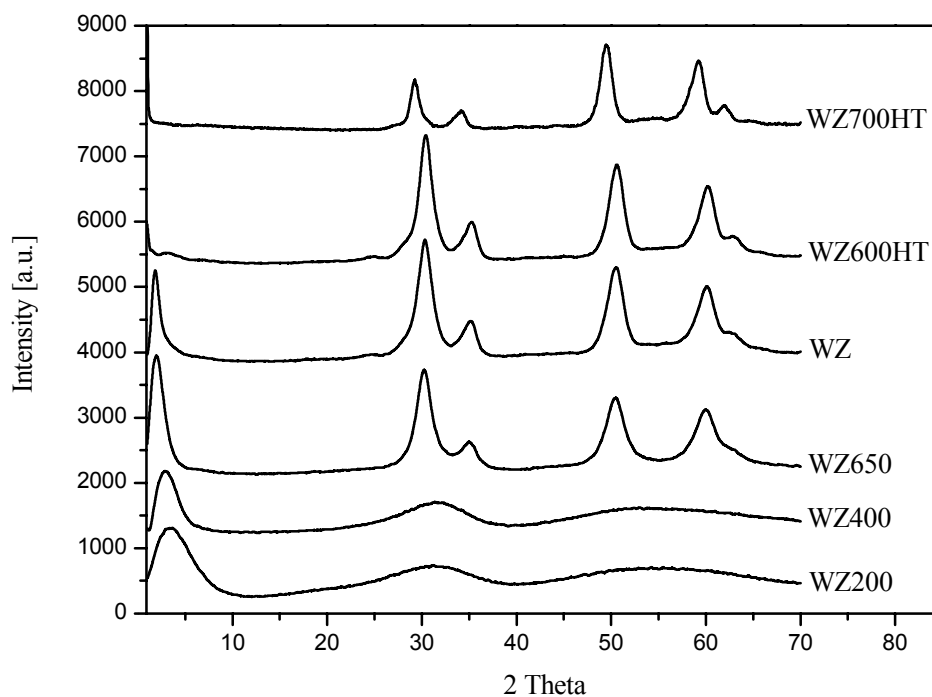
where  $\lambda$  is the wavelength of the X-Ray,  $B$  is the full width at half maximum (in radian) of the reflection,  $\theta_B$  is the position of the reflection in the XRD pattern and  $t$  is the crystal size. Not only the crystallite size causes the broadening of the reflection peak but also the instrumental broadening causes. Slit widths, sample size, penetration in the sample, imperfect focusing and unresolved  $\alpha_1$  and  $\alpha_2$  peaks of the source are the reason of the instrumental broadening. Instrumental peak broadening can be determined by using a very big crystal of the sample. Since crystal size effect on the peak broadening is removed due to the large crystallite

size of the sample, the full width at half maximum of the reflection band comes from the instrumental sources. So the peak broadening due to instrumental sources is removed. Si sample with 2000 nm crystallite size was used in order to determine instrumental broadening because big crystal of the sample of our interest is not possible. According to this method, the instrumental broadening is about  $0.1^\circ$ .

The crystallite size of tetragonal  $ZrO_2$  phase was calculated 4.7 nm after the subtraction of the instrumental peak broadening.

The sample calcined at 773 K for 5 h (WZ) is still a mixture of tetragonal  $ZrO_2$  phase and randomly oriented mesoporous  $ZrO_2$  phase (Fig. 4). The peak at low angle shifts to the left until the heat treatment at 873 K. This means that an opening of pores takes place. The peak intensities of tetragonal  $ZrO_2$  phase for WZ are higher than those for WZ 650. Contrary, the intensity of the peak at  $1.8^\circ$  for WZ decreases relative to that of the peak at  $2^\circ$  for WZ 650. It indicates that after calcination, there is a simultaneous increase in the amount of the tetragonal  $ZrO_2$  phase and decrease in the amount of the mesoporous phase. The tetragonal crystallite size is 4.9 nm for WZ. There is a small crystallite size difference between WZ 650 and WZ. It can be concluded that the presence of tungsten oxide and mesoporous phase stabilizes tetragonal  $ZrO_2$  crystallites and retard the growth of  $ZrO_2$  grains. This is consistent with the literature data [66-68].

Powder X-ray diffraction patterns of the heat treated samples (WZ600HT and WZ700HT) show that samples contain only crystalline tetragonal zirconia phase and the intensity of the peak at low angle belonging to mesoporous phase decreases considerably for WZ600HT and disappears completely for WZ700HT. It means that the mesoporous phase is not stable and pores collapse at high temperature. Furthermore the crystallite size of the tetragonal zirconia phase increases.



**Figure 4.** Effects of the heating at 473 K and at 673 K, carbonization at 923 K, calcination at 773 K and heat treatments at 873 K and at 973 K on the X-ray diffraction patterns during the preparation of the tungstated zirconia sample.

### 3. 1. 1. 2. Zirconia

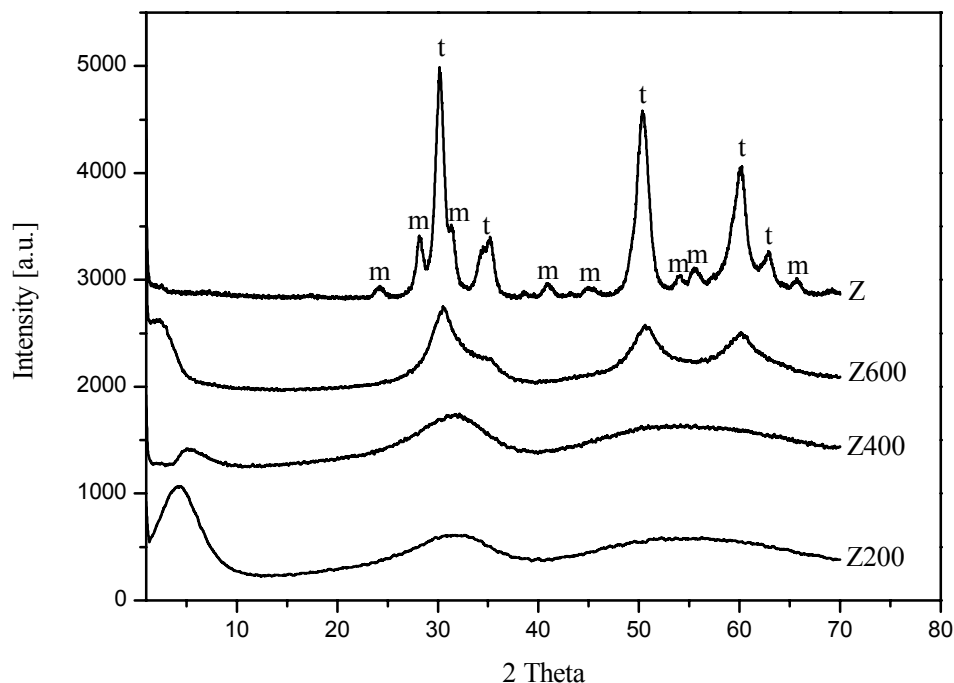
The X-ray diffraction pattern of the heated sample at 673 K, denoted by Z 400, shows one broad peak at  $5.1^\circ$  and two broad features in the range of  $2\theta$  from 22 to  $40^\circ$  and from 40 to  $70^\circ$  (Fig. 5). The broad peaks show that the sample has a very low degree of crystallinity. There is a mesoporous phase in the sample, which can be determined from the peak at low angle [64].

The diffractogram of the carbonized sample at 873 K, designated by Z 600, reveals that it consists of crystalline tetragonal zirconia phase and randomly distributed mesoporous phase.

The sample calcined at 773 K for 5 h, represented by Z, is a mixture of tetragonal and monoclinic  $ZrO_2$  phases (Fig. 5). The peak at low angle shifts to the left after each heat treatment. It means that pore widening takes place. The peak intensity of mesoporous phase for Z decreases sharply. It can be concluded

that most of the mesoporous phase disappears and/or pores collapse at 773 K. The crystallite size of the tetragonal phase is 7.7 nm for Z.

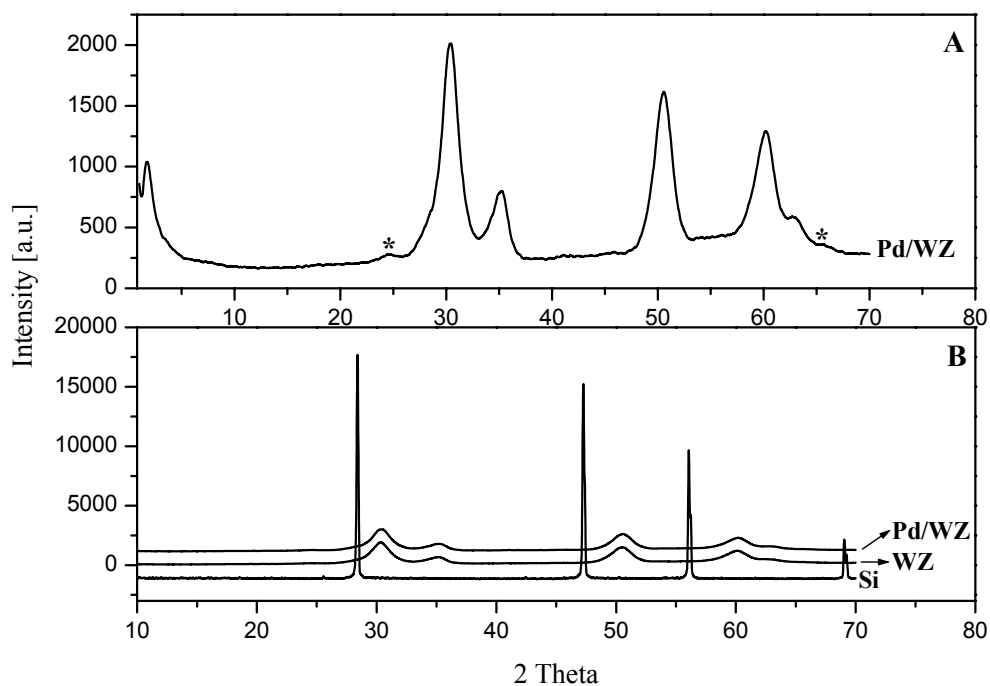
The crystallographic phase compositions were calculated by using the Toraya et al. [69]. Then, the volume percentage of the tetragonal zirconia is 39%.



**Figure 5.** Effects of the heating at 473 K and at 673 K, carbonization at 873 K and calcination at 773 K on the X-ray diffraction patterns during the preparation of the pure zirconia sample (t: tetragonal, m: monoclinic).

### 3. 1. 1. 3. Palladium modified Tungstated zirconia

Diffraction pattern of Pd impregnated on tungstated zirconia shows that it contains the crystalline tetragonal zirconia phase and randomly distributed mesoporous phase. But phase transformation from tetragonal to monoclinic has started in the sample, which can be differentiated from the appearance of the small peaks in Fig. 6.



**Figure 6.** A: X-ray diffraction pattern after the preparation of Pd modified tungstated zirconia sample (\* indicates the monoclinic phase). B: X-ray diffraction patterns of the sample for comparison.

### 3. 1. 2. Tungsten Density

Theoretically the atomic ratio of Zr to W (Zr:W) was chosen 8.25:1, corresponding to 18.6% of  $\text{WO}_3$  by a mass content. This corresponds to nominal surface density of  $2.8 \text{ WO}_3/\text{nm}^2$ , which is 0.5 of the monolayer. The coverage is obtained by using the maximum packing density of planar  $\text{WO}_3$  species equal to  $0.21 \text{ g WO}_3/100\text{m}^2$  [42].

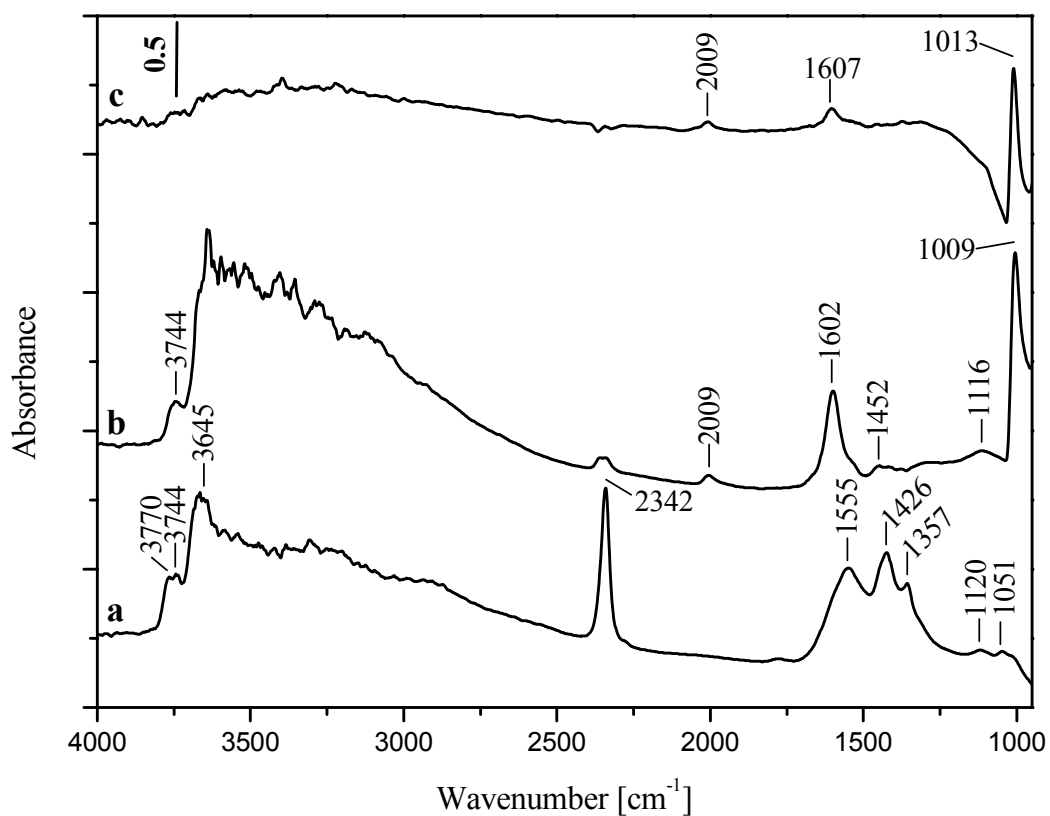
### 3. 1. 3. FT-IR Spectra of the Activated Samples

Fig. 7 shows FT-IR spectra of the activated Pd/WZ catalyst (spectrum c), WZ support (spectrum b) together with pure zirconia (spectrum a). The activated spectrum of the  $\text{ZrO}_2$  in the OH-stretching region displays a pair of bands at  $3770$  and  $3744 \text{ cm}^{-1}$ , strong absorption at  $3645 \text{ cm}^{-1}$  and a broad band

between 3500 and 3000  $\text{cm}^{-1}$ . According to the literature data [29,61,70], the band at 3770  $\text{cm}^{-1}$  is attributed to terminal OH-groups due to the monoclinic phase. The band at 3744  $\text{cm}^{-1}$  belongs to bibridged OH-groups and the band at 3645  $\text{cm}^{-1}$  is assigned to tribridged OH groups from the monoclinic and tetragonal phases. The broad band is attributed to H-bonded tribridged hydroxyls. The band at 2342  $\text{cm}^{-1}$  corresponds to adsorbed  $\text{CO}_2$  [69]. Bolis et al. [71] reported that relatively stable  $\text{CO}_2$  adsorbed on tetragonal zirconia resisting room temperature evacuation. The bands in the 1700 - 1100  $\text{cm}^{-1}$  region are assigned to surface carbonates [70]. Most probably  $\text{CO}_2$  appears as a product of the decomposition of the residual carbonates (produced from burning of the sample and adsorb on the surface when the temperature is lowered).

The spectrum of the tungstated zirconia sample (Fig. 7, spectrum b) in the OH-stretching region is characterized by the bands corresponding to bibridged terminal OH-groups (3744  $\text{cm}^{-1}$ ) [29] and tribridged terminal hydroxyls (3645  $\text{cm}^{-1}$ ) of the tetragonal zirconia. An intense band at 1009  $\text{cm}^{-1}$  due to  $\nu(\text{W}=\text{O})$  and the respective overtone at 2009  $\text{cm}^{-1}$  [72,73] are observed. These bands are typical of wolframyl species ( $\text{W}^{6+}=\text{O}$ ) supported on zirconia [73]. The broad band in the 3600-3000  $\text{cm}^{-1}$  region and band at 1602  $\text{cm}^{-1}$  are due to adsorbed water, which requires prolonged activation in order to remove. The bands in the 1550 - 1100  $\text{cm}^{-1}$  region are assigned to surface carbonates [29,70].

The spectrum of Pd/WZ catalyst is similar to that of WZ. The amount of adsorbed water is lower and no surface carbonates are observed.



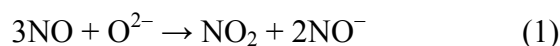
**Figure 7.** FT-IR spectra of the activated zirconia (a), WZ sample (b) and Pd/WZ catalyst (c). The spectra are taken at ambient temperature.

### 3. 2. NO and NO/O<sub>2</sub> Adsorption and Thermal Stability of the Adsorbed NO<sub>x</sub> species

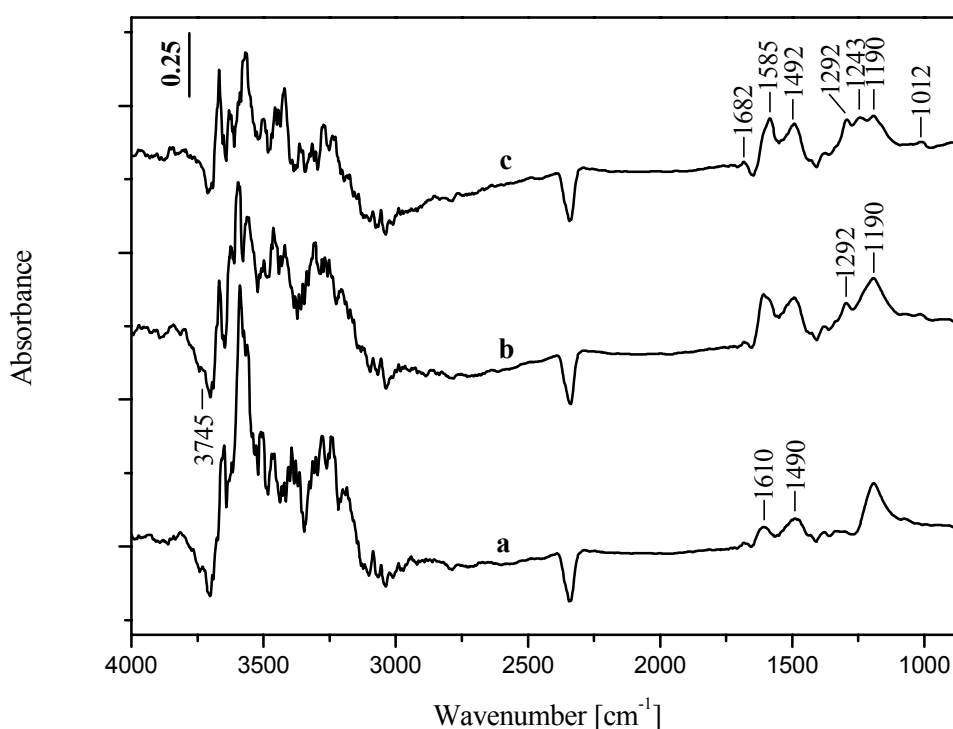
#### 3. 2. 1. Adsorption of NO

##### 3. 2. 1. 1. Adsorption of NO at Room Temperature on ZrO<sub>2</sub>

Spectra of NO (1.34kPa) adsorbed at room temperature on the zirconia sample for a period of 20 min are shown in Fig. 8. The intense band at 1190 cm<sup>-1</sup> (Fig. 8, spectrum b) is assigned to the  $\nu(\text{NO})$  stretching mode of anionic nitrosyl, NO<sup>-</sup> [61]. These species can form by disproportionation NO on the surface O<sup>2-</sup> sites:



The  $\text{NO}_2$  produced can be adsorbed on the surface, leading to formation of  $\text{NO}_3^-$  and  $\text{NO}_2^-$  species (bands in the  $1600\text{-}1000\text{ cm}^{-1}$  region) [61,62,74]. The presence of adsorbed  $\text{NO}_x$  species causes perturbation of the isolated OH groups at  $3745\text{ cm}^{-1}$  and appearance of hydrogen-bonded hydroxyls. The weak band  $1682\text{ cm}^{-1}$  is assigned to *cis*- $\text{HNO}_2$  [61].



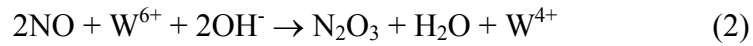
**Figure 8.** FTIR spectra of adsorbed NO (1.34 kPa) on pure zirconia sample at room temperature immediately (a), for 20 min (b), and after evacuation (c). The spectrum of the activated sample is used as a background reference.

### 3. 2. 1. 2. Adsorption of NO on WZ at Room Temperature

Spectra of NO (1.34 kPa) adsorbed at room temperature on the WZ sample are shown in the Fig. 9. The equilibrium between the gaseous NO and the adsorbed  $\text{NO}_x$  species is established after 10 min. The band at  $1180\text{ cm}^{-1}$  is attributed to  $\nu_{\text{as}}(\text{NO}_2)$  mode of bidentate nitrito species [62]. The pair of bands at  $1455$  and  $1425\text{ cm}^{-1}$  are assigned to the  $\nu_{\text{as}}(\text{NO}_2)$  modes of two types of



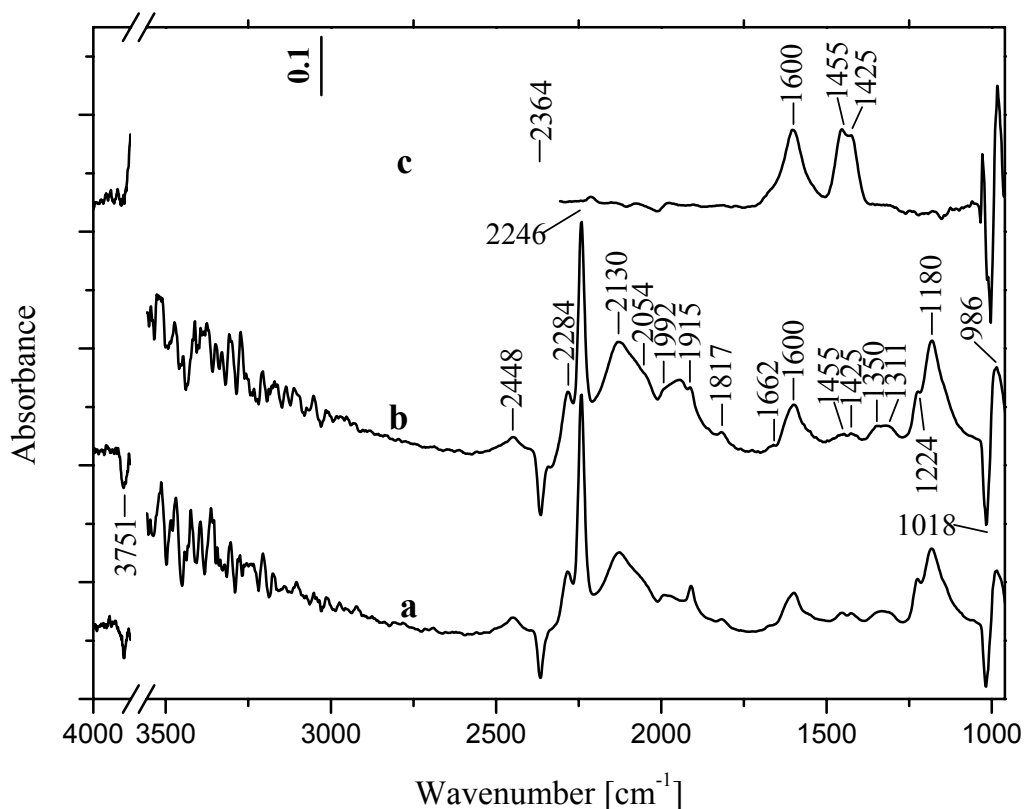
monodentate nitro species [62]. This assignment is consistent with the fact that they resist evacuation at room temperature (see Fig. 9, spectrum c). In general, the nitro species are more stable than the nitrito species. The  $\nu_s(\text{NO}_2)$  modes of the nitro and nitrito species fall below  $1100\text{ cm}^{-1}$  and cannot be detected. The fact that  $\text{NO}_2^-$  species are formed indicates that the adsorbed NO undergoes oxidation. Since  $\text{Zr}^{4+}$  ions are considered to be unreducible under these conditions, the following process, in which the surface hydroxyls at  $3751\text{ cm}^{-1}$  and  $\text{W}^{6+}$  ions are involved, can be suggested:



Indeed, appearance of a negative band at  $3751\text{ cm}^{-1}$  and the positive absorption in the  $3500 - 3000\text{ cm}^{-1}$  support the participation of the  $\text{Zr}^{4+}\text{-OH}$  groups in this process leading to formation of adsorbed water molecules ( $\delta(\text{H}_2\text{O})$  at  $1600\text{ cm}^{-1}$ ). The bands at  $2054$  and  $\sim 1992\text{ cm}^{-1}$  together with the weak absorption at  $1350$  and  $1311\text{ cm}^{-1}$  correspond to the  $\nu(\text{N=O})$  and  $\nu_s(\text{NO}_2)$  modes of  $\text{N}_2\text{O}_3$  adsorbed on two different sites [59,74]. The  $\nu_{\text{as}}(\text{NO}_2)$  stretching vibration is overlapped by the water band at  $1600\text{ cm}^{-1}$ . It can be proposed that  $\text{N}_2\text{O}_3$  undergoes self-ionization according to the reaction:

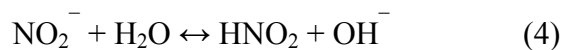


The  $\text{NO}^+$  species are identified by the absorption band at  $2130\text{ cm}^{-1}$  due to the  $\nu(\text{NO})$  mode [59,61]. Most probably the  $\text{NO}_2^-$  species obtained in this process are the bidentate nitrites at  $1180\text{ cm}^{-1}$ . They disappear together with the adsorbed  $\text{N}_2\text{O}_3$  and  $\text{NO}^+$ , which confirms the occurrence of the equilibrium (3). The bands at  $2284$  and  $2246\text{ cm}^{-1}$  are assigned to the  $\nu(\text{NN})$  modes of  $\text{N}_2\text{O}$  adsorbed on two different sites [59,74]. The  $\nu(\text{NO})$  stretching vibration is at  $1224\text{ cm}^{-1}$ . The weak band at  $2446\text{ cm}^{-1}$  is due to the first overtone of the  $\nu(\text{NO})$  fundamental band of  $\text{N}_2\text{O}$ . Since no  $\text{Zr}^{4+}\text{-NO}$  bands are observed on the pure zirconia (see page 23, Fig. 8), the absorption at  $1915\text{ cm}^{-1}$  is attributed to Zr(IV) species, of which wolframyl groups are in their vicinity.



**Figure 9.** FTIR spectra of adsorbed NO (1.34 kPa) on the WZ support at room temperature immediately (a), for 10 min (b), and after evacuation at room temperature for 15 min. The spectrum of the activated sample is used as a background reference.

The weak band at  $1662\text{ cm}^{-1}$  is assigned to the  $\nu(\text{N}=\text{O})$  modes of adsorbed cis- $\text{HNO}_2$  molecules [61], which are produced by interaction of the  $\text{NO}_2^-$  species with the adsorbed water:



An assignment of the IR bands observed upon NO adsorption on the WZ support is summarized in Table 5.

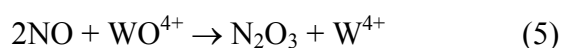
**Table 5.** Assignments of the FT-IR bands observed upon NO adsorption on the WZ support.

NO <sub>x</sub> species	Band Position (cm <sup>-1</sup> )	Mode
NO <sup>+</sup>	2130	v(NO)
H <sub>2</sub> O	1600 3751	δ(H <sub>2</sub> O) v(OH)
cis-HNO <sub>2</sub>	1662	v(N=O)
Bidentate nitrito, NO <sub>2</sub> <sup>-</sup>	1180	v <sub>as</sub> (NO <sub>2</sub> )
Monodentate nitro, NO <sub>2</sub> <sup>-</sup> (two types)	1455 1425	v <sub>as</sub> (NO <sub>2</sub> )
N <sub>2</sub> O <sub>3</sub> (two different sites)	2054, 1992 1350, 1311 1600	v(N=O) v <sub>s</sub> (NO <sub>2</sub> ) v <sub>as</sub> (NO <sub>2</sub> )
N <sub>2</sub> O (two different sites)	2284, 2246 1224 2446	v(NN) v(NO) 2v(NO)
Zr <sup>4+</sup> -NO	1915	v(NO)

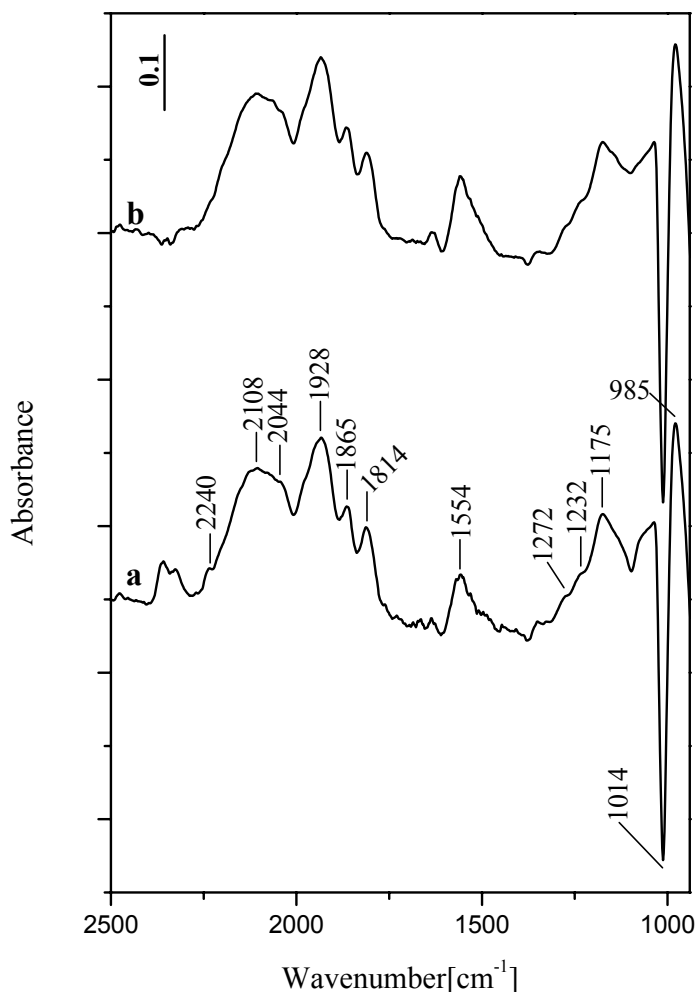
### 3. 2. 1. 3. Adsorption of NO on Pd/WZ at Room Temperature

Spectra of adsorbed NO (1.34 kPa) on the Pd/WZ catalyst at room temperature are similar to those observed for the tungstated zirconia. Following differences should be noticed:

1. There are no Zr<sup>4+</sup>-NO nitrosyls.
2. The bands at 1863 and 1810 cm<sup>-1</sup> are due to NO adsorbed on two different Pd(II) sites [75,76].
3. The adsorbed N<sub>2</sub>O<sub>3</sub> (1935 and 1558 cm<sup>-1</sup>) and the nitrito species at 1166 cm<sup>-1</sup> resist the evacuation. Since the surface OH groups are not perturbed, the following process leading to N<sub>2</sub>O<sub>3</sub> formation can be proposed:



Involvement of the wolframyl species is confirmed by the appearance of a negative band at 1012 cm<sup>-1</sup>.

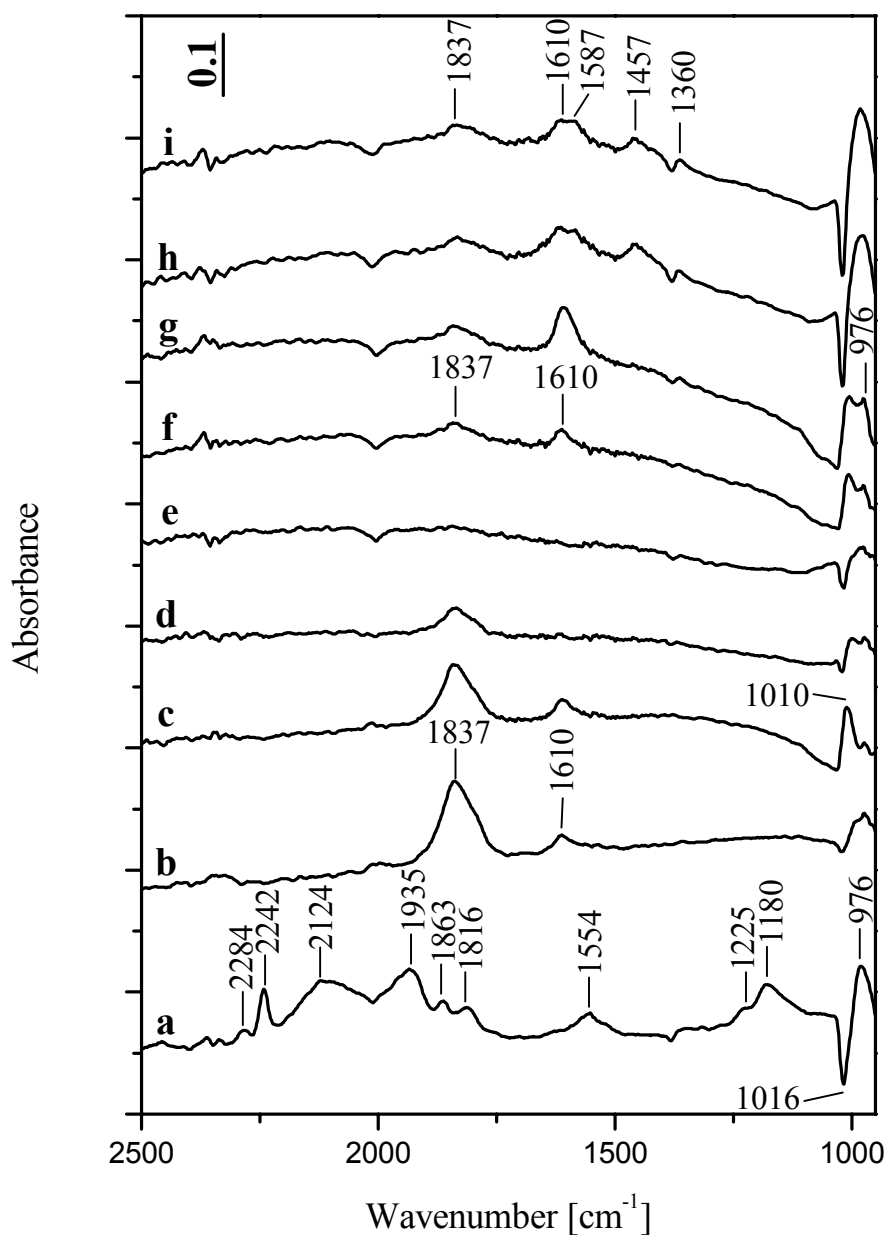


**Figure 10.** FT-IR spectra of adsorbed NO (1.34 kPa) on the Pd/WZ catalyst at room temperature for 40 min (a) and after evacuation (b). The spectrum of the activated sample is used as a background reference and the gas phase spectra are subtracted.

### 3. 2. 1. 4. High Temperature Adsorption of NO on the Pd/WZ Catalyst

Figure 11 shows the spectrum of the Pd/WZ catalyst taken after adsorption of NO (1.33 kPa) for 15 min (spectrum a) at room temperature, followed by heating the closed IR cell for 15 min at 623 K (spectrum b). The latter treatment causes all of the NO<sub>x</sub> species observed at room temperature to disappear. Two new bands at 1837 and 1790 cm<sup>-1</sup> (shoulder) and weak band at 1610 cm<sup>-1</sup> are detected. The gas phase spectrum recorded at 623 K (not shown)

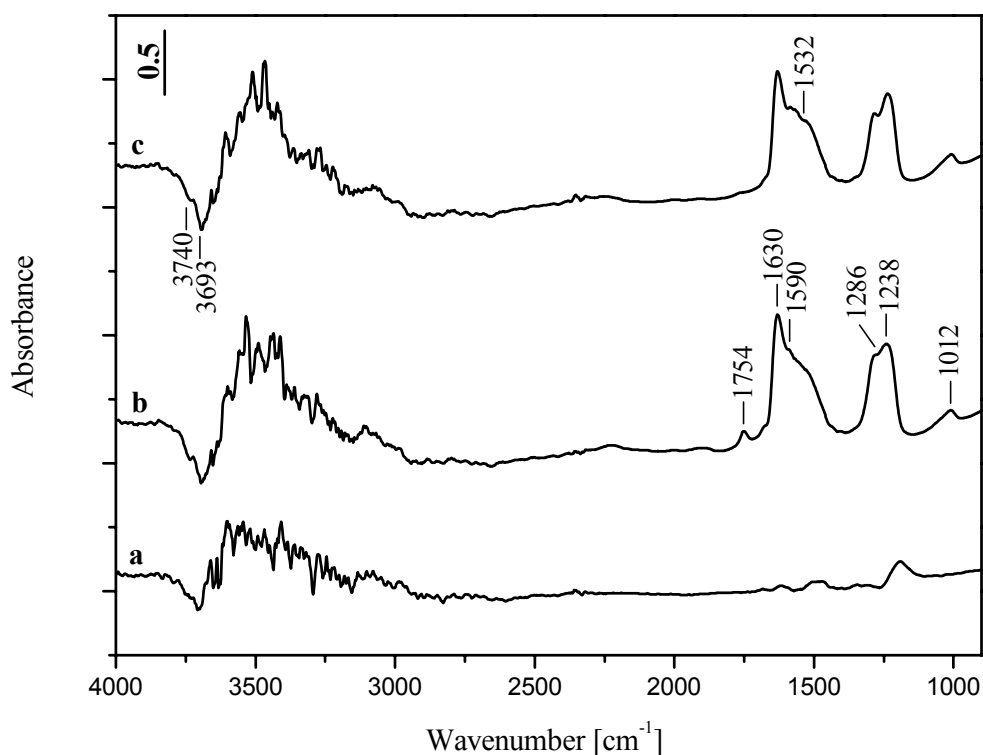
contains  $\text{NO}_2$  in addition to  $\text{NO}$ . Some amount of  $\text{N}_2\text{O}$  is also detected, which was formed already at room temperature. Based on this, the band at  $1610\text{ cm}^{-1}$  in spectrum b (Fig. 11) is attributed to adsorbed  $\text{NO}_2$ . This experimental fact shows that oxidation of  $\text{NO}$  to  $\text{NO}_2$  has occurred. In this process the  $\text{Pd}^{2+}$  sites are involved because the  $\text{W}^{6+}=\text{O}$  species are almost completely restored, whereas strong perturbation in the region of the  $\text{Pd}^{2+}-\text{NO}$  nitrosyls is observed. The weak bands at  $1863$  and  $1816\text{ cm}^{-1}$  corresponding to two types of  $\text{Pd}^{2+}-\text{NO}$  nitrosyls have disappeared and considerably stronger bands at  $1837$  and at about  $1790\text{ cm}^{-1}$  (shoulder) are observed instead. These two bands are assigned to two different  $\text{Pd}^+-\text{NO}$  linear species, which correspond to the  $\text{Pd}^{2+}-\text{NO}$  nitrosyls observed at room temperature. The  $\text{Pd}^+-\text{NO}$  nitrosyls display high thermal stability and do not disappear upon evacuation at  $623\text{ K}$  (Fig. 11, spectrum c). Increasing the temperature of the closed IR cell to  $773\text{ K}$  (Fig. 11, spectra d and e) leads first to removal of the adsorbed  $\text{NO}_2$  and then to loss of  $\text{NO}$  adsorbed on the  $\text{Pd}^+$  sites. Cooling back to room temperature (Fig. 11, spectra from f to h) causes reappearance of  $\text{Pd}^+-\text{NO}$  bands with reduced intensities, which indicates further oxidation of the adsorbed  $\text{NO}$ . The intensity of the band due to the adsorbed  $\text{NO}_2$  ( $1610\text{ cm}^{-1}$ ) increases with lowering the temperature, reaching maximum at  $523\text{ K}$ . This band disappears at room temperature due to conversion of the adsorbed  $\text{NO}_2$  to surface nitrate and nitro species ( $1610$ ,  $1587$ ,  $1457$  and  $1360\text{ cm}^{-1}$ ).



**Figure 11.** FT-IR spectra of the Pd/WZ sample taken after adsorption of NO (1.33 kPa) at room temperature for 15 min (a), after heating of the closed IR cell for 15 min at 623 K (b), and subsequent evacuation for 15 min at 623 K (c) then continuing heating the closed IR cell for 15 min at 723 K (d), at 773 K (e). Afterwards the closed IR cell was cooled to 623 K (f) to 523 K (g) and to RT (h). The spectrum of the activated sample is used as a background reference and the gas phase spectra are subtracted.

### 3. 2. 2. Coadsorption of NO/O<sub>2</sub> and Thermal Stability of NO<sub>x</sub> produced

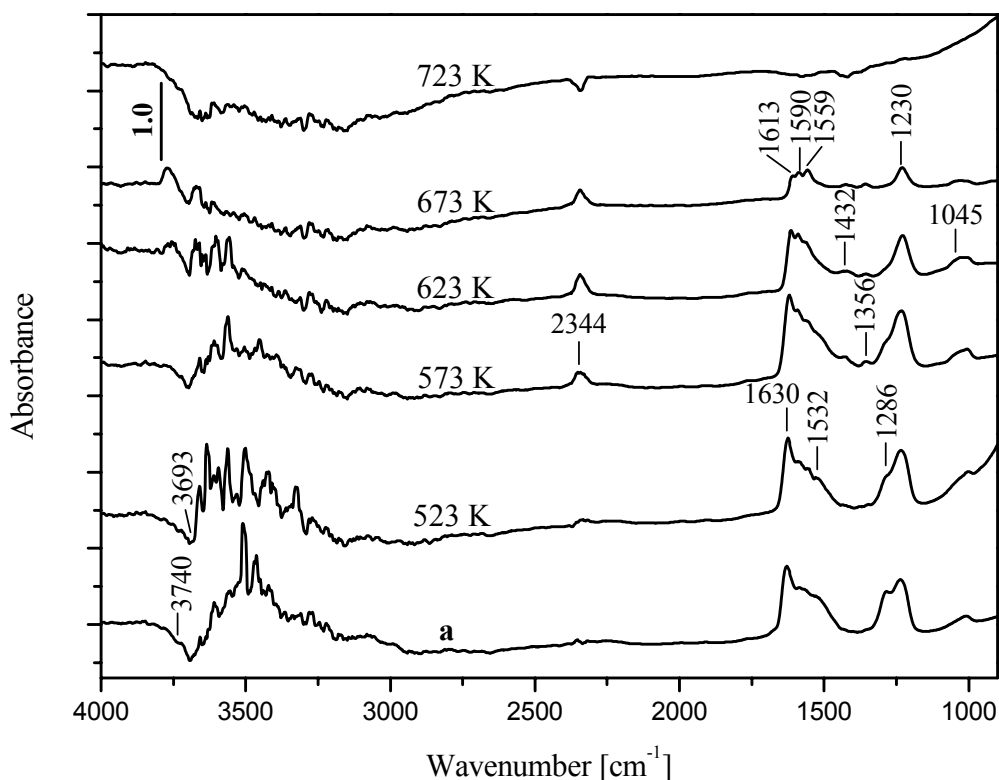
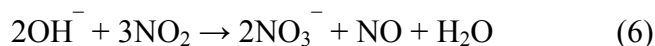
#### 3. 2. 2. 1. On the ZrO<sub>2</sub> Sample



**Figure 12.** FT-IR spectra of NO (1.34 kPa) adsorbed on the zirconia support at room temperature for 10 min (a), after subsequent introduction of O<sub>2</sub> (2.66 kPa) for 35 min (b), and after evacuation for 15 min at ambient temperature (c). The spectrum of the activated sample is used as a background reference.

Fig. 12 shows the spectra of the zirconia support obtained after the adsorption of 1.34 kPa of NO for 10 min (Fig. 12, spectrum a). Subsequent addition of 2.66 kPa of O<sub>2</sub> to the IR cell for 35 min (Fig. 12, spectrum b) causes formation of NO<sub>2</sub> (the color of the gas phase has changed to brown) and disappearance of the band at 1190 cm<sup>-1</sup> corresponding to the ionic nitrosyl. The band at 1754 cm<sup>-1</sup>, which disappears after the evacuation at room temperature, is characteristic of adsorbed N<sub>2</sub>O<sub>4</sub> [59]. The strong bands between 1650 and 1200 cm<sup>-1</sup> correspond to various surface nitrates. The increase in the intensities of the

negative bands at 3740 and 3693  $\text{cm}^{-1}$ , which is accompanied by appearance of positive absorption in the region of the H-bonded OH groups, suggests that the surface nitrates are formed by disproportionation of  $\text{NO}_2$  with the involvement of the isolated surface hydroxyls [77,78]:



**Figure 13.** FT-IR spectra obtained after adsorption of  $\text{NO}/\text{O}_2$  at RT followed by evacuation for 10 min (a), after heating the zirconia containing adsorbed  $\text{NO}_x$  species for 15 min in vacuum. The spectra are recorded after cooling of the IR cell to the room temperature. The spectrum of the activated sample is used as a background reference.

The nitrate species resist room-temperature evacuation (Fig. 12, spectrum c). However, heating the  $\text{NO}_x$ -precovered sample under vacuum in the 523 – 573 K temperature range (Fig. 13, spectra b and c) causes disappearance mainly of the monodentate nitrates at 1532 and 1286  $\text{cm}^{-1}$  [59]. The bidentate



(1630, 1590 and 1233  $\text{cm}^{-1}$ ) nitrates display higher thermal stability and disappear from the spectrum after dynamic evacuation at 723 K [59,62].

The assignment of the IR bands observed upon NO/O<sub>2</sub> coadsorption on the zirconia sample is summarized in Table 6.

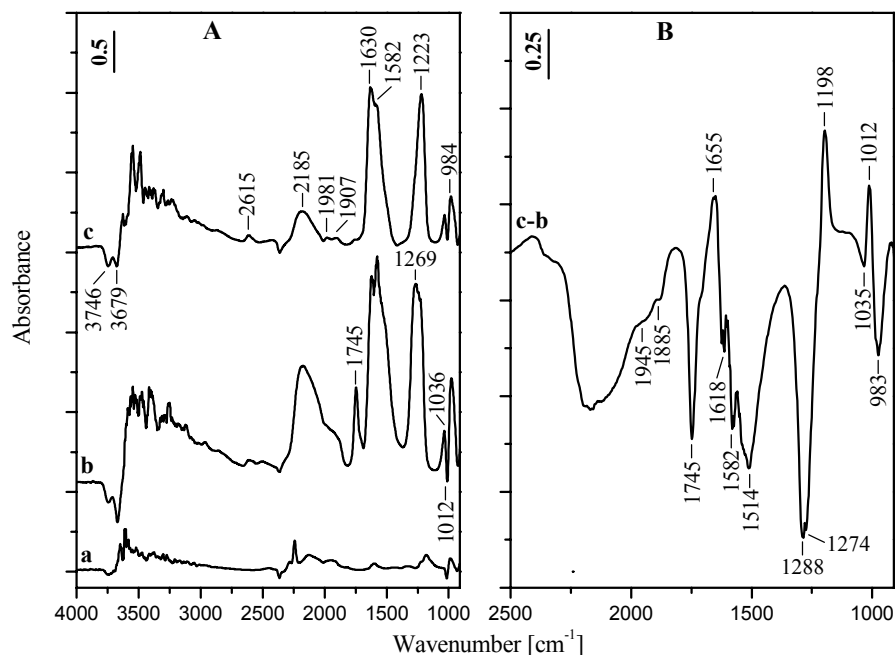
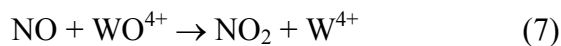
**Table 6.** Assignments of the FT-IR bands observed upon NO/O<sub>2</sub> coadsorption on the zirconia sample.

<b>NO<sub>x</sub> species</b>	<b>Band Position (<math>\text{cm}^{-1}</math>)</b>	<b>Mode</b>
Monodentate NO <sub>3</sub> <sup>-</sup>	1532	$\nu_{\text{as}}(\text{NO}_2)$
	1286	$\nu_{\text{s}}(\text{NO}_2)$
Bidentate NO <sub>3</sub> <sup>-</sup>	1630-1613,1590,1559	$\nu(\text{N}=\text{O})$
	1230	$\nu_{\text{as}}(\text{NO}_2)$
N <sub>2</sub> O <sub>4</sub>	1754	$\nu(\text{N}=\text{O})$

### 3. 2. 2. 2. On the WZ Support

Figure 14 shows the spectra of the WZ support obtained after the adsorption of 1.34 kPa of NO for 10 min (Fig. 14A, spectrum a), followed by the addition of 2.66 kPa of O<sub>2</sub> to the IR cell for 30 min (Fig. 14A, spectrum b). Compared to the pure zirconia, the amount of the adsorbed species observed in the presence of the gas phase is considerably larger. The weakly adsorbed species, which disappear after evacuation at room temperature (Fig. 14B), are identified as follows (see Table 7 for the assignment of the bands): N<sub>2</sub>O<sub>3</sub> adsorbed on two different sites (1945, 1885, 1582, 1514, 1288 and 1274  $\text{cm}^{-1}$ ), N<sub>2</sub>O<sub>4</sub> (1745 and 1288  $\text{cm}^{-1}$ ) and NO<sub>2</sub> (1618  $\text{cm}^{-1}$ ) [59,78]. The strong band at 2185  $\text{cm}^{-1}$ , which decreases in intensity after the evacuation, is typical of NO<sup>+</sup> species. Formation of large amounts of oxides of nitrogen with oxidation numbers +3 and +4, which is not observed in the case of NO/O<sub>2</sub> adsorption on pure zirconia, suggests that in the oxidation of NO not only O<sub>2</sub> but also the wolframyl, W<sup>6+</sup>=O, species are involved. This is confirmed by the appearance of a negative band at 1012  $\text{cm}^{-1}$

(shifted to  $984\text{ cm}^{-1}$ ) due to perturbed wolframyl groups. The following processes can be proposed:



**Figure 14.** (A) FT-IR spectra of NO (1.34 kPa) adsorbed on the WZ support at room temperature for 10 min (a), after subsequent introduction of O<sub>2</sub> (2.66 kPa) for 30 min (b), and after evacuation for 10 min at ambient temperature (c). The spectrum of the activated sample is used as a background reference. (B) FT-IR subtraction spectra of the WZ sample obtained from the spectra drawn in A.

As in the case of pure zirconia, the bands at 1630, 1582 and  $1223\text{ cm}^{-1}$  resisting the evacuation correspond to bidentate nitrates. They can form by both disproportionation (reaction 6) and self-ionization of NO<sub>2</sub>/N<sub>2</sub>O<sub>4</sub> [61]:



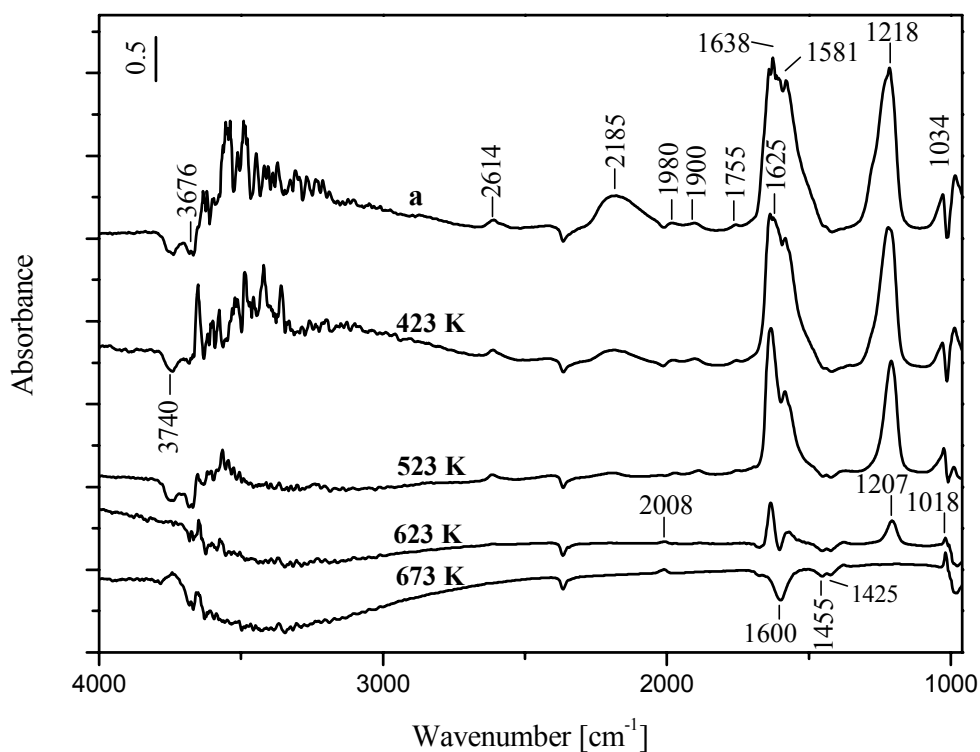
The weak bands at 2615, 1981, and 1907  $\text{cm}^{-1}$  (Fig. 14A, spectrum c) correspond to combination modes of the fundamental nitrate bands.

**Table 7.** Assignments of the FT-IR bands observed upon NO/O<sub>2</sub> coadsorption on the WZ support.

Species	Band, $\text{cm}^{-1}$	Mode
NO <sup>+</sup>	2185	$\nu(\text{NO})$
N <sub>2</sub> O <sub>4</sub>	1745,	$\nu_{\text{as}}(\text{NO}_2)$
	1288	$\nu_{\text{s}}(\text{NO}_2)$
N <sub>2</sub> O <sub>3</sub>	1945, 1885	$\nu(\text{N=O})$
	1582, 1514	$\nu_{\text{as}}(\text{NO}_2)$
	1288, 1274	$\nu_{\text{s}}(\text{NO}_2)$
NO <sub>2</sub>	1618	$\nu_{\text{as}}(\text{NO}_2)$
Monodentate NO <sub>3</sub> <sup>-</sup>	1514	$\nu_{\text{as}}(\text{NO}_2)$
	1274	$\nu_{\text{s}}(\text{NO}_2)$
	1035	$\nu(\text{N=O})$
Bidentate NO <sub>3</sub> <sup>-</sup>	1630, 1582	$\nu(\text{N=O})$
	1223	$\nu_{\text{as}}(\text{NO}_2)$
	1755	$\nu_{\text{s}}(\text{NO}_2) + \delta(\text{ONO})$
	2614	$\nu(\text{N=O}) + \nu_{\text{s}}(\text{NO}_2)$

The thermal stability of the adsorbed NO<sub>3</sub><sup>-</sup> species is lower than that on pure zirconia. They disappear after the evacuation at 673 K (Fig. 15). The negative absorption in the 3600 – 3000  $\text{cm}^{-1}$  region and the band at 1600  $\text{cm}^{-1}$  observed in the spectra d and e (Fig. 15) are due to desorbed water molecules initially present in the activated sample. The weak negative bands at 1455 and 1425  $\text{cm}^{-1}$  indicate that there is a loss in the carbonate species present as

contaminations on the surface of the WZ sample. The adsorbed  $\text{NO}_x$  species facilitate desorption of adsorbed water and carbonate impurities, which were difficult to remove during the activation of the sample.

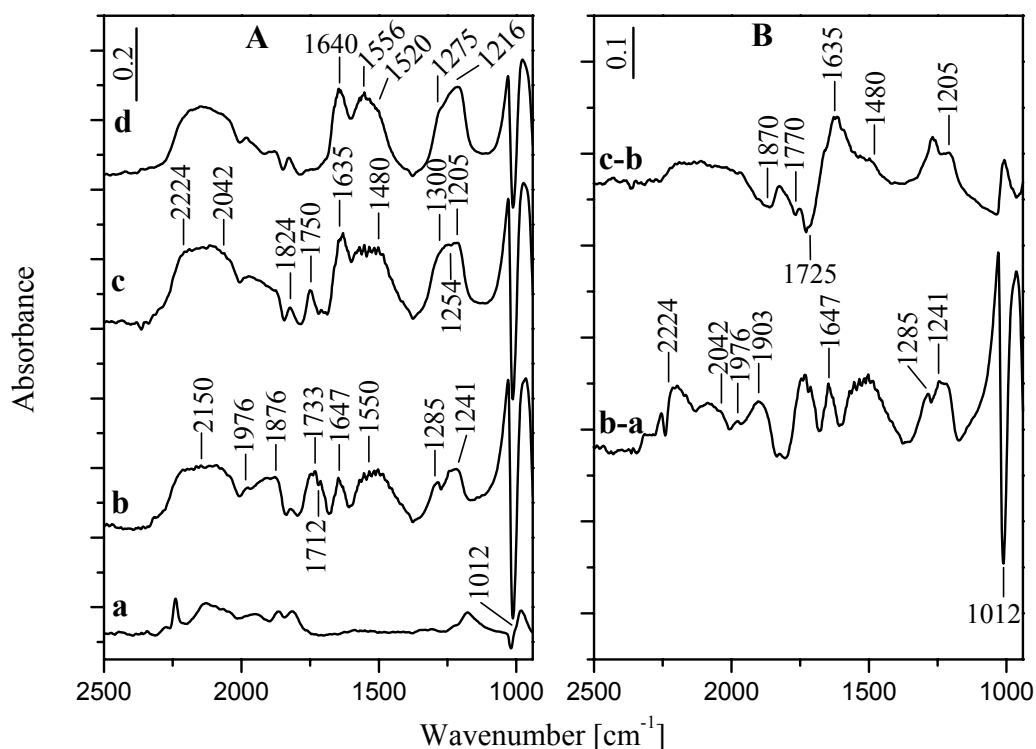


**Figure 15.** FT-IR spectra obtained after adsorption of  $\text{NO}/\text{O}_2$  at RT followed by evacuation for 10 min (a), after heating the WZ sample containing adsorbed  $\text{NO}_x$  species for 15 min in vacuum. The spectra are recorded after cooling of the IR cell to the room temperature. The spectrum of the activated sample is used as a background reference.

### 3. 2. 2. 3. On the Pd/WZ Catalyst

Figure 16 shows the spectra of the Pd/WZ sample recorded after the adsorption of 1.34 kPa of  $\text{NO}$  for 25 min (Fig. 16A, spectrum a), followed by the addition of 2.66 kPa of  $\text{O}_2$  to the IR cell for 30 min (Fig. 16A, spectrum b). The spectrum of adsorbed  $\text{NO}/\text{O}_2$  shows new bands in the region between 1800 and 1200  $\text{cm}^{-1}$  (subtraction spectrum b-a in Fig. 16B). During the  $\text{NO}/\text{O}_2$  adsorption no change in the  $\nu(\text{OH})$  stretching region is observed in the spectra. The gas phase

spectrum (corresponding to the conditions of spectrum b) shows the formation of  $\text{N}_2\text{O}_3$  and  $\text{N}_2\text{O}_4/\text{NO}_2$  [59,74,78]. These gases adsorb (see also the subtraction spectrum b-a in Fig. 16B) on the surface producing bands at 1910 and 1876  $\text{cm}^{-1}$  ( $\text{N}_2\text{O}_3$ ) and 1750 and 1712  $\text{cm}^{-1}$  ( $\text{N}_2\text{O}_4$  adsorbed on two different sites). The  $\nu(\text{N}=\text{O})$  mode of the  $\text{N}_2\text{O}_3$  overlaps the  $\text{Pd}^{2+}\text{-NO}$  band at 1876  $\text{cm}^{-1}$  [75,76]. As in the case of the WZ sample (see Section 3.2.2.2) the absorption at 1976  $\text{cm}^{-1}$  corresponds to the  $\nu(\text{NO})$  stretching vibration in the complex  $\text{ON-Zr}^{4+}\text{-ONO}_2^-$  [61]. The broad band with maximum at about 2160  $\text{cm}^{-1}$  reveals the presence of  $\text{NO}^+$  ions. These species can be produced by self-ionization of the adsorbed  $\text{N}_2\text{O}_4$  with the participation of Lewis acid-base pairs according to reaction (6).

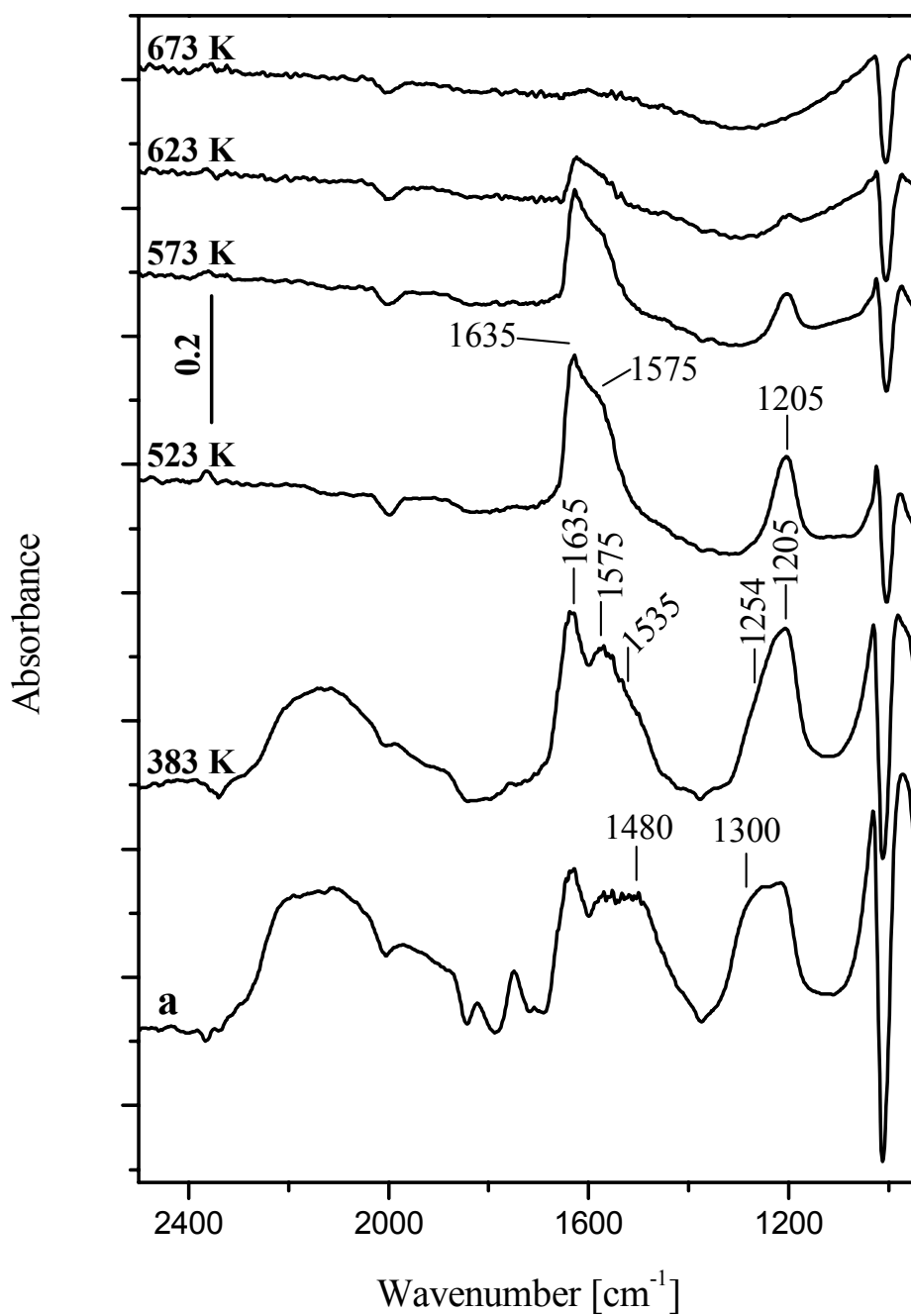


**Figure 16.** (A) FT-IR spectra of NO (1.34 kPa) adsorbed on the Pd/WZ catalyst at room temperature for 25 min (a), after subsequent introduction of  $\text{O}_2$  (2.66 kPa) for 30 min (b), after evacuation for 10 min (c) and for 30 min (d) at ambient temperature. The spectrum of the activated sample is used as a background reference and the gas phase spectra are subtracted. (B) FT-IR subtraction spectra of the Pd/WZ sample obtained from the spectra drawn in A.

The nitrate species are identified by the band at  $1647\text{ cm}^{-1}$  due to the  $\nu(\text{N}=\text{O})$  stretching vibration (bridging coordination mode) [62]. The characteristic stretching vibrations of the bidentate and monodentate nitrates species fall in the  $1600 - 1400$  and  $1300 - 1200\text{ cm}^{-1}$  regions and cannot be resolved. The negative band at  $1012\text{ cm}^{-1}$  indicates strong perturbation of the  $\text{W}^{6+}=\text{O}$  species. The band at  $1020\text{ cm}^{-1}$ , which is offset by the negative band at  $1012\text{ cm}^{-1}$ , is due to the  $\nu_s(\text{NO}_2)$  modes of the nitrate species. The subtraction spectrum b-a in Fig. 16 shows loss in the intensities of the  $\text{Pd}^{2+}-\text{NO}$  bands at  $1876$  and  $1824\text{ cm}^{-1}$ , which most probably is due to replacement of the adsorbed NO by the nitrate species. The evacuation for 10 min at room temperature (Fig. 16A, spectrum c and Fig. 16B, spectrum c-b) causes removal of  $\text{N}_2\text{O}_3$  (negative band at  $1870\text{ cm}^{-1}$ ) and decrease in the intensity of the bands associated with adsorbed  $\text{N}_2\text{O}_4$  (negative bands at  $1750$  and  $1725\text{ cm}^{-1}$ ). This is accompanied by increase in the intensities of the bands due to the charged species ( $\text{NO}^+$  and  $\text{NO}_3^-$ ) indicating that the evacuation favors the self-ionization of the  $\text{N}_2\text{O}_4$ . Extending the evacuation to 30 min (Fig. 16, spectrum d) causes almost complete removal of the adsorbed  $\text{N}_2\text{O}_4$  and decrease in the intensity of the broad band due to  $\text{NO}^+$  ions.

Upon evacuation for 10 min in the  $383 - 623\text{ K}$  temperature range the broad absorption bands in the nitrate region loose intensities (Fig. 17). By using the subtraction spectra (not shown) it is found that the adsorbed  $\text{N}_2\text{O}_4$  and the monodentate nitrates characterized by the bands at  $1469$  and  $1295\text{ cm}^{-1}$  desorb first from the surface. Increasing the temperature to  $523\text{ K}$  causes removal of the monodentate nitrates at  $1535$  and  $\sim 1254\text{ cm}^{-1}$ . The species characterized by the broad absorption between  $1650$  and  $1500\text{ cm}^{-1}$  with a concomitant band at  $1205\text{ cm}^{-1}$  display the highest thermal stability. They are attributed to bidentate nitrates species [59]. The corresponding absorption bands are observed with reduced intensities at  $623\text{ K}$  and disappear upon the evacuation at  $673\text{ K}$ . The thermal stability of the surface nitrates formed upon  $\text{NO}/\text{O}_2$  adsorption at room temperature on the WZ and Pd/WZ samples is comparable.

The assignment of the FT-IR bands is shown in Table 8.



**Figure 17.** FT-IR spectra obtained after adsorption of  $\text{NO}/\text{O}_2$  at RT followed by evacuation for 10 min (a), after heating the Pd/WZ sample containing adsorbed  $\text{NO}_x$  species for 10 min in vacuum. The spectrum of the activated sample is used as a background reference and the gas phase spectra are subtracted.

**Table 8.** Assignments of the FT-IR bands observed upon NO/O<sub>2</sub> coadsorption on the Pd/WZ catalyst.

Species	Band, cm <sup>-1</sup>	Mode
NO <sup>+</sup>	2160	v(NO)
Pd <sup>2+</sup> – NO	1876, 1824	v(NO)
ON – Zr <sup>4+</sup> – NO <sub>3</sub> <sup>-</sup>	1976	v(NO)
N <sub>2</sub> O <sub>4</sub>	1750, 1712	v <sub>as</sub> (NO <sub>2</sub> )
	1285	v <sub>s</sub> (NO <sub>2</sub> )
N <sub>2</sub> O <sub>3</sub>	1910, 1876	v(N=O)
	1469	v <sub>as</sub> (NO <sub>2</sub> )
	1295	v <sub>s</sub> (NO <sub>2</sub> )
Monodentate NO <sub>3</sub> <sup>-</sup> (two types)	1469, 1535	v <sub>as</sub> (NO <sub>2</sub> )
	1295, 1254	v <sub>s</sub> (NO <sub>2</sub> )
Bidentate NO <sub>3</sub> <sup>-</sup>	1650, 1500	v(N=O)
	1205	v <sub>as</sub> (NO <sub>2</sub> )
	1020	v <sub>s</sub> (NO <sub>2</sub> )

### 3. 2. 3. Summary of the Results on NO and NO/O<sub>2</sub> Adsorption on the Samples Studied

Adsorption of NO reveals the presence of coordinatively unsaturated Zr<sup>4+</sup> ions on the tungstated zirconia. No such sites are observed on Pd/WZ catalyst.

The surface NO<sub>x</sub> species observed during the room temperature adsorption of NO on WZ and Pd/WZ samples are produced by the involvement of the W<sup>6+</sup>=O groups. The Pd(II) sites interact with NO upon heating at 623 K giving rise to adsorbed NO<sub>2</sub>.

It is also observed that the stabilities of nitrito species and N<sub>2</sub>O<sub>3</sub> are different on WZ and Pd/WZ samples. Even though adsorbed N<sub>2</sub>O<sub>3</sub> and nitrito species on the WZ sample leave easily the surface upon evacuation at room temperature, those species on the Pd/WZ catalyst resist desorption upon evacuation. So the presence of Pd<sup>2+</sup> changes the behavior of the species observed commonly on both samples.



Coadsorption of NO and O<sub>2</sub> at room temperature results in formation of various surface nitrates and gaseous species; e.g. NO<sub>2</sub>, N<sub>2</sub>O<sub>4</sub>, N<sub>2</sub>O<sub>3</sub>. Oxidation of NO is due to O<sub>2</sub> and the wolframyl groups present on the samples. Nitrates and nitrosonium ions are observed on the WZ and Pd/WZ because of the self-ionization of N<sub>2</sub>O<sub>4</sub>. Evacuation in the 383-623 K temperature range shows that the surface nitrates have similar thermal stabilities for both samples. This and the lower surface concentration of the nitrate species show that in the case of the Pd/WZ catalyst they are coordinated to the support.

### **3. 3. Reactivity of the Adsorbed Coadsorption of NO/O<sub>2</sub> and Thermal Stability of NO<sub>x</sub> produced**

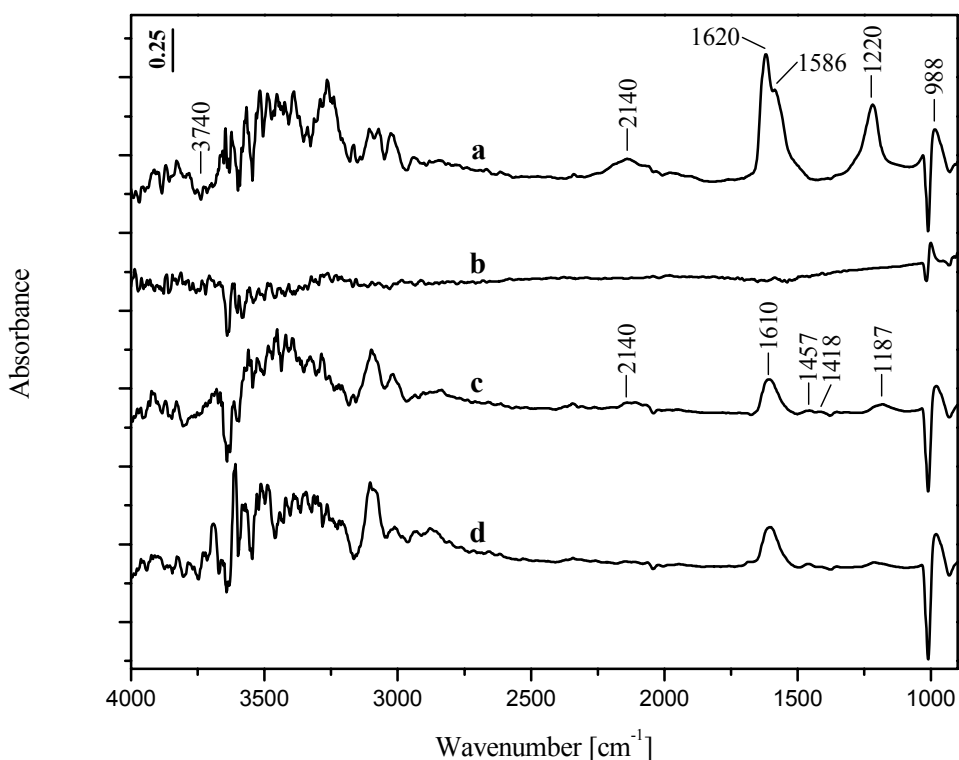
In order to evaluate the ability of the catalyst containing preadsorbed NO<sub>x</sub> species for methane activation, the following experiments were performed:

- (i) “Blank NO<sub>x</sub>” experiment involves the formation of NO<sub>x</sub> adsorbed species by NO/O<sub>2</sub> coadsorption, followed by evacuation at room temperature and heating the closed IR cell containing the NO<sub>x</sub>-precovered catalyst at 723 K.
- (ii) “Blank CH<sub>4</sub>” experiment, which consists of interaction of the activated catalyst with methane at elevated temperatures.
- (iii) “NO<sub>x</sub> - CH<sub>4</sub>” experiment involves the interaction of methane with the catalyst containing preadsorbed NO<sub>x</sub> species at various temperatures.

#### **3. 3. 1. “Blank NO<sub>x</sub>” Experiment**

##### **3. 3. 1. 1. With The WZ Support**

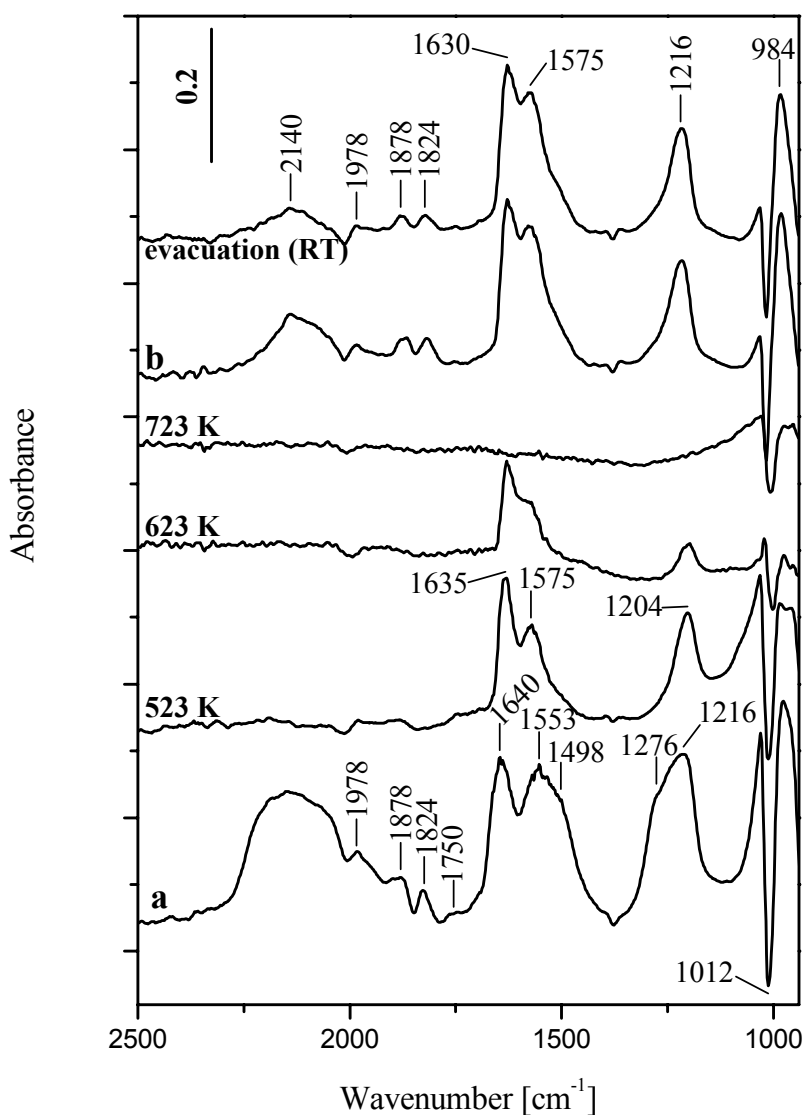
Heating the closed IR cell for 20 min at 723 K (Fig. 18, spectrum b) causes complete removal of the adsorbed NO<sub>x</sub> species. After cooling to room temperature (spectrum c) bands due to readsorbed NO<sup>+</sup> ions (2140 cm<sup>-1</sup>) and bidentate nitrates (1610 and 1187 cm<sup>-1</sup>) are detected. The weak bands at 1457 and 1418 cm<sup>-1</sup> indicate the presence of NO<sub>2</sub><sup>-</sup> (monodentate nitrito or bridged nitro) species.



**Figure 18.** FT-IR spectra of the WZ support taken after adsorption of NO/O<sub>2</sub> mixture (1.33 kPa : 2.66 kPa, NO:O<sub>2</sub> = 1:2) at ambient temperature followed by evacuation down to  $3 \times 10^{-3}$  Torr (a), after heating of the closed IR cell for 20 min at 723 K (b), then cooling of it to RT (c), and then evacuation of the gas phase at RT (d). The spectrum of the activated sample is used as a background reference.

This experimental fact shows that decomposition of the surface nitrates has occurred. However, due to the low partial pressures of the decomposition products (NO<sub>2</sub>, NO and O<sub>2</sub>), they were not detected in the gas phase spectrum. This could be the reason that the adsorbed NO<sub>x</sub> species are not completely restored. Another possible explanation is that some of the surface nitrates undergo decomposition to N<sub>2</sub> and O<sub>2</sub>. However, in order to confirm this assumption, further experiments are needed.

### 3. 3. 1. 2. With The Pd/WZ Catalyst



**Figure 19.** FT-IR spectra of the Pd/WZ sample taken after adsorption of NO/O<sub>2</sub> mixture (1.33 kPa : 2.66 kPa, NO:O<sub>2</sub> = 1:2) at room temperature followed by evacuation for 30 min (a), after heating of the closed IR cell for 15 min, then cooling to RT (b). The spectrum of the activated sample is used as a background reference and the gas phase spectra are subtracted.

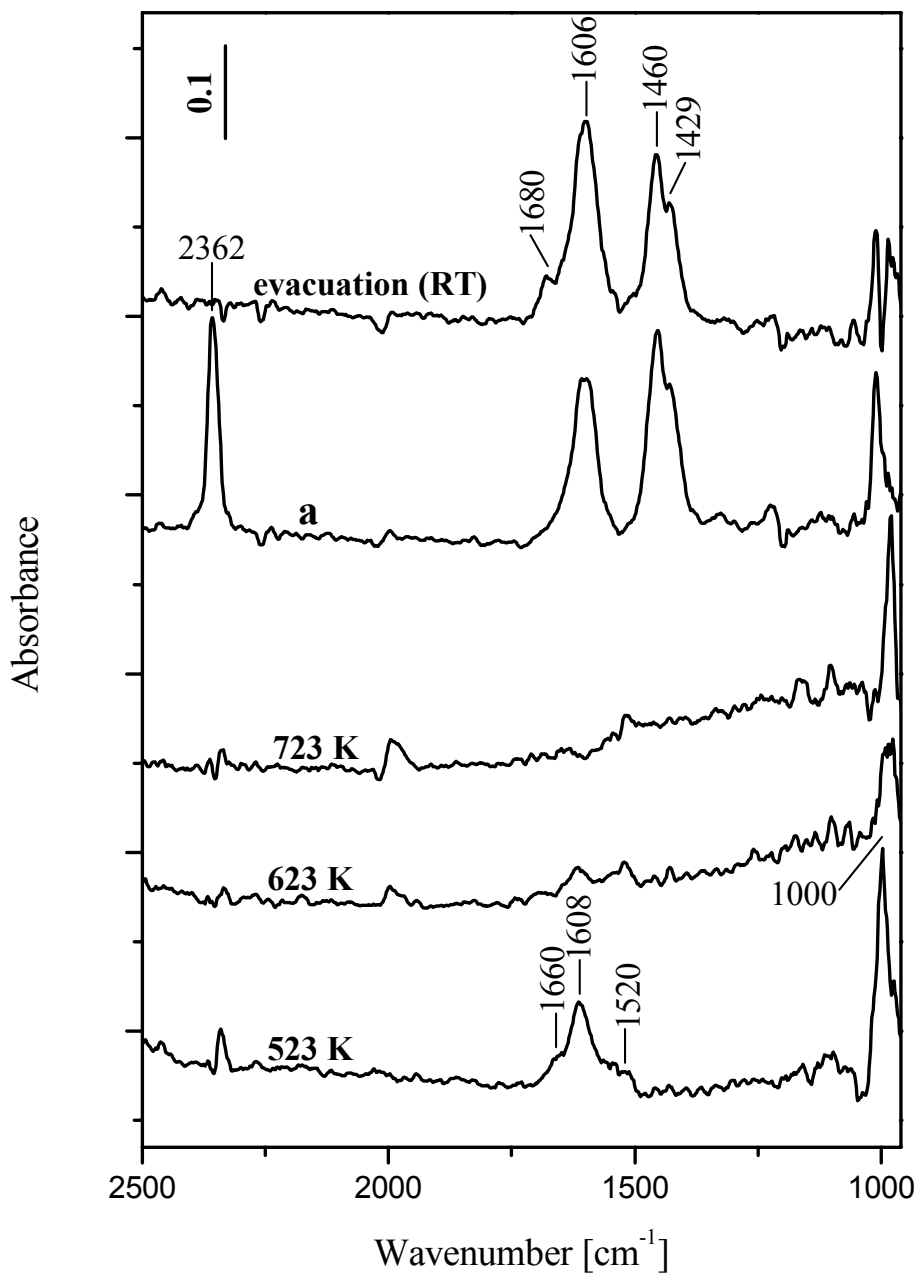
The preadsorbed NO<sub>x</sub> species are created on the surface of the Pd/WZ catalyst by exposing 1.33 kPa of NO and 2.66 kPa of O<sub>2</sub> (NO:O<sub>2</sub> = 1:2) for 30 min followed by evacuation for 30 min at room temperature (Fig. 19, spectrum a). Heating the closed IR cell for 15 min at 523 K leads to disappearance of the NO<sup>+</sup>

species ( $2140\text{ cm}^{-1}$ ), nitrate-nitrosyl complex ( $1978\text{ cm}^{-1}$ ),  $\text{Pd}^{2+}$  – NO nitrosyls ( $1878$  and  $1824\text{ cm}^{-1}$ ) and monodentate nitrates ( $1498$ ,  $1276$ ). Complete removal of the adsorbed  $\text{NO}_x$  species occurs under heating the closed IR cell at  $723\text{ K}$  (Fig. 19, spectrum at  $723\text{ K}$ ). The increase in the temperature causes decrease in the intensity of the negative band at  $1010\text{ cm}^{-1}$  due to restoration of perturbed  $\text{W}^{6+}=\text{O}$  groups. However, the restored wolframyl species differ from the original ones, which is evident by the blue shift of the  $\nu(\text{W}=\text{O})$  band from  $1009$  to  $1023\text{ cm}^{-1}$  (Fig. 19, spectrum at  $723\text{ K}$ ). Moreover, cooling the IR cell to room temperature (Fig. 19, spectrum b) results in reappearance of the  $\text{NO}^+$  ions ( $2140\text{ cm}^{-1}$ ),  $\text{Pd}^{2+}$ –NO nitrosyls ( $1878$  and  $1824\text{ cm}^{-1}$ ) and bidentate nitrates (bands with maxima at  $1630$ ,  $1575$  and  $1216\text{ cm}^{-1}$ ). The amount of the perturbed  $\text{W}^{6+}=\text{O}$  species increases again as a result of the readsorption of the gaseous phase.

### 3. 3. 2. “Blank $\text{CH}_4$ ” Experiment

#### 3. 3. 2. 1. With The WZ Support

Results of heating the activated WZ support under constant pressure of methane ( $8\text{ kPa}$ ) in the closed IR cell in the temperature range  $523 - 723\text{ K}$  are shown in Fig. 20. The oxidation of  $\text{CH}_4$  starts already at  $523\text{ K}$  (Fig. 20, spectrum a), which is evident by appearance of weak bands in the carbonate-carboxylate region [70] at  $1660$ ,  $1608$  and about  $1520\text{ cm}^{-1}$ . Increasing the temperature to  $723\text{ K}$  the corresponding adsorption forms disappear from the spectra. The spectrum obtained after cooling to room temperature contains strong band at  $2362\text{ cm}^{-1}$  typical of adsorbed  $\text{CO}_2$  [70]. In the low-frequency region the band at  $1606\text{ cm}^{-1}$  reveals the formation of bidentate carbonates, whereas the pair of bands at  $1460$  and  $1429\text{ cm}^{-1}$  can be assigned to two types of monodentate carbonates [70]. The weak bands at  $1680$  and  $1230\text{ cm}^{-1}$  are typical of hydrogencarbonates [70]. All of the bands except that of  $\text{CO}_2$  resist the room-temperature evacuation, which is in agreement with their assignments. The data show that the WZ sample is able to catalyze the complete oxidation of the  $\text{CH}_4$ . Taking into account the fact that



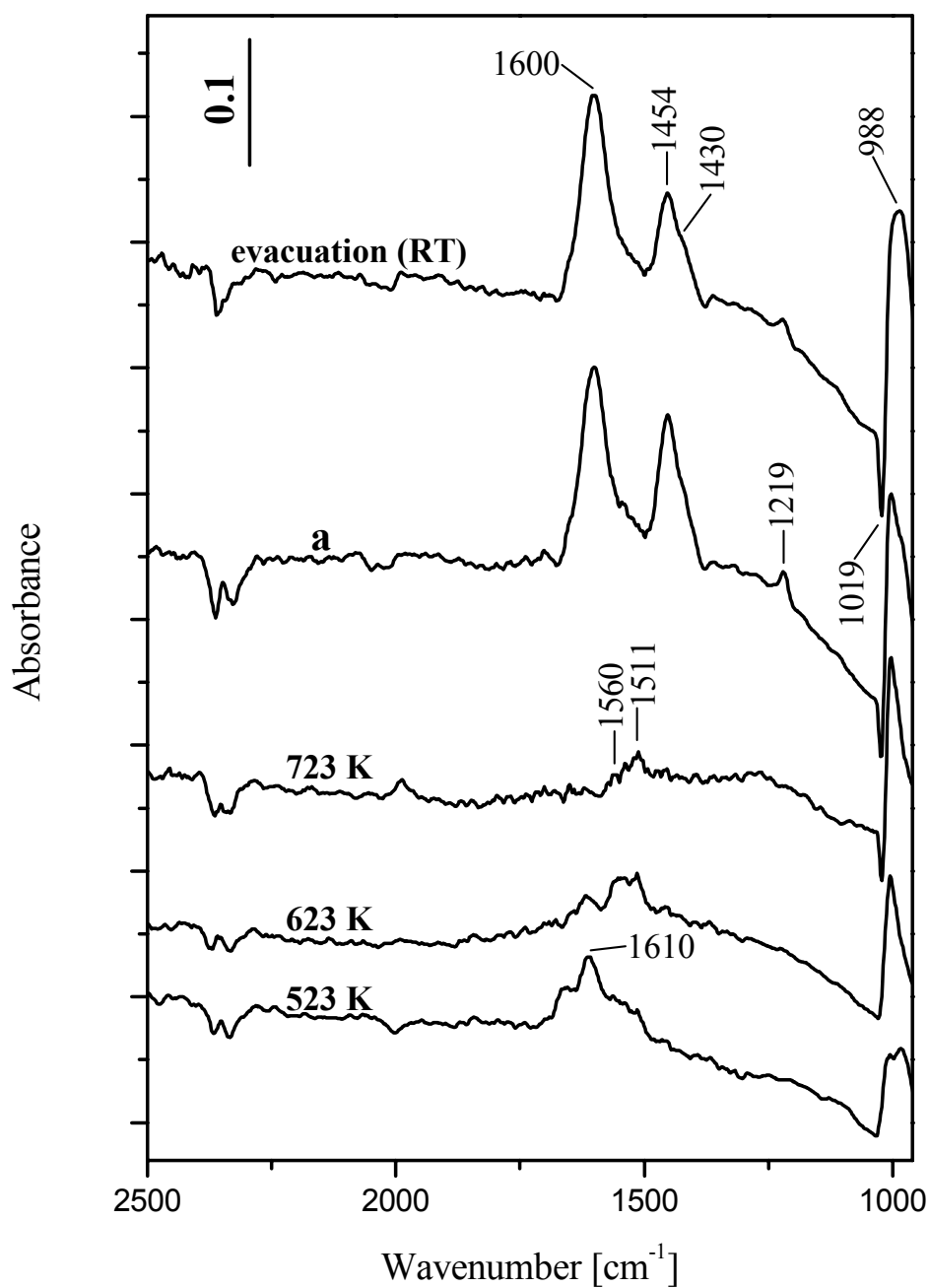
**Figure 20.** FT-IR spectrum of the WZ support taken after addition of methane (8 kPa) at room temperature, followed by heating of the closed IR cell for 20 min. Then cooling to RT (a). The spectrum of the activated sample is used as a background reference and the gas phase spectra are subtracted.

zirconia is unreducible below 900 K [79], the oxidation of methane can be caused by the oxide ions coordinated to the tungsten(VI) species. This results in perturbation of the wolframyl groups (positive absorption at  $1000\text{ cm}^{-1}$ ).

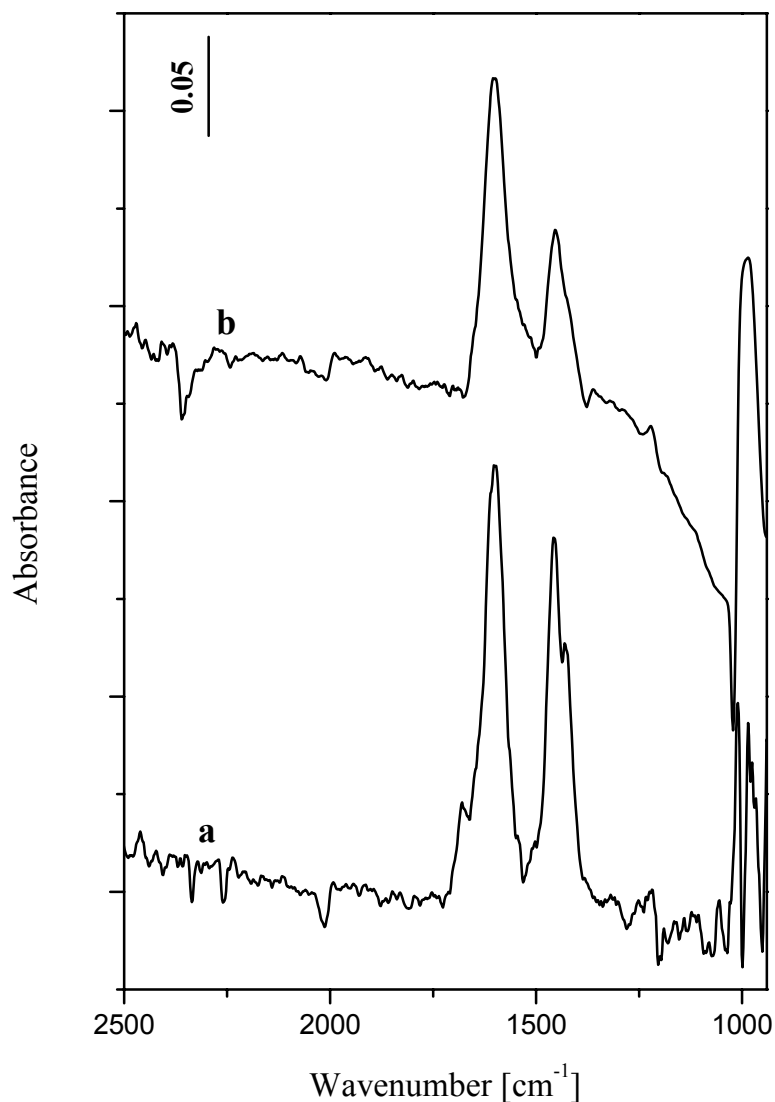
### 3.3.2.2. With The Pd/WZ Catalyst

Heating of the activated Pd/WZ catalyst in the presence of methane (constant pressure of 8 kPa) in the temperature range 523 – 723 K results in appearance of bands similar to those detected on the WZ support. Noticeable difference is the higher thermal stability of the carbonates formed on the surface of the Pd/WZ catalyst: bidentate carbonate bands at  $1560$  and  $1511\text{ cm}^{-1}$  are detected at 723 K. This can be due to coordination of the carbonate species to reduced palladium sites. As in the case of the WZ sample, the spectra obtained after cooling to room temperature (Fig. 21, spectrum a) and after evacuation (in Fig. 21) contain bands corresponding to bidentate ( $1600\text{ cm}^{-1}$ ), monodentate ( $1454$  and  $1430\text{ cm}^{-1}$ ) and hydrogen-carbonates ( $1640$  and  $1219\text{ cm}^{-1}$ ). Since it is well known that Pd(II)-containing catalysts are very active in the complete oxidation of methane, it is reasonable to conclude that both Pd(II) and W(VI) are involved in this process.

Figure 22 compares the spectra of the WZ and the Pd/WZ taken from the blank  $\text{CH}_4$  experiment after the final evacuation at room temperature. Fig. 22 indicates that the amount of the surface carbonates on the WZ is higher than that on the Pd/WZ.



**Figure 21.** FT-IR spectrum of the Pd/WZ sample taken after addition of methane (8 kPa) at room temperature and followed by heating of the closed IR cell for 15 min. Then cooling to RT (a). The spectrum of the activated sample is used as a background reference and the gas phase spectra are subtracted.



**Figure 22.** FT-IR spectra taken from “Blank CH<sub>4</sub>” experiment after the final evacuation at room temperature for the WZ sample (a) and for the Pd/WZ sample (b).

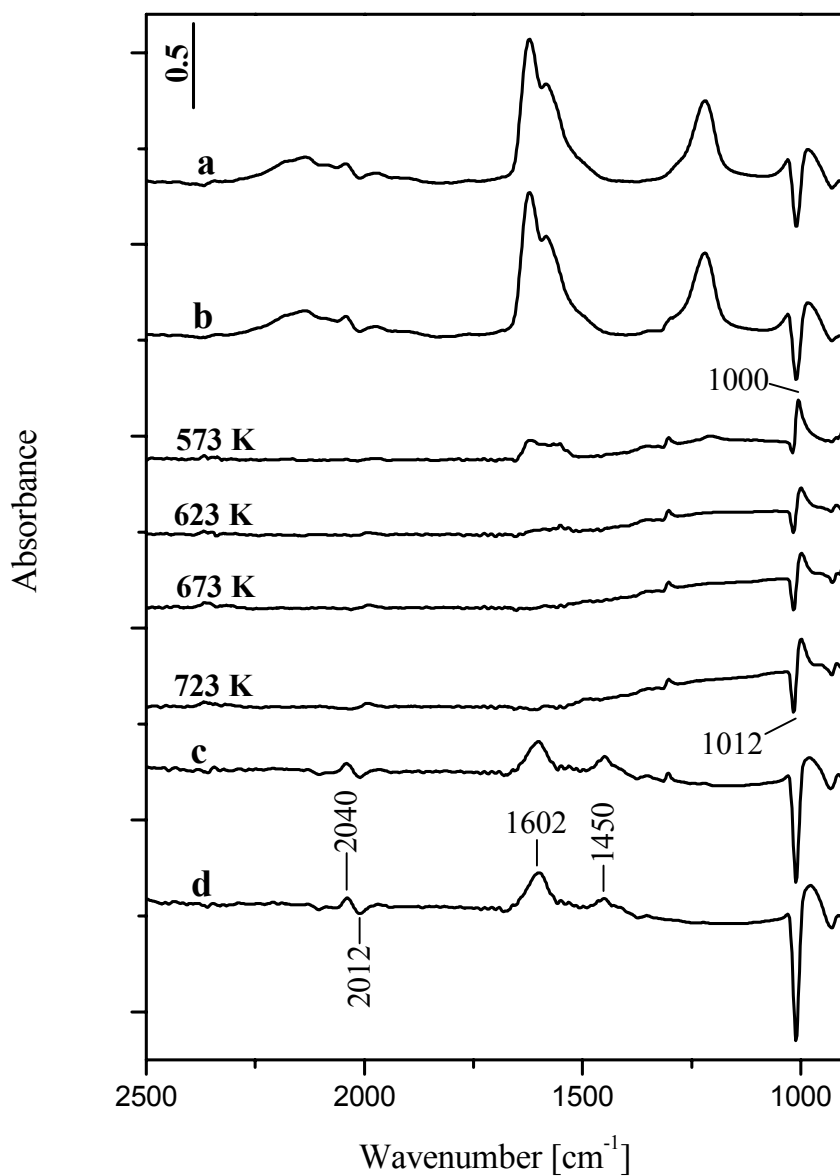
### 3. 3. 3. Interaction of Preadsorbed NO<sub>x</sub> species with Methane

#### 3. 3. 3. 1. On The WZ Support

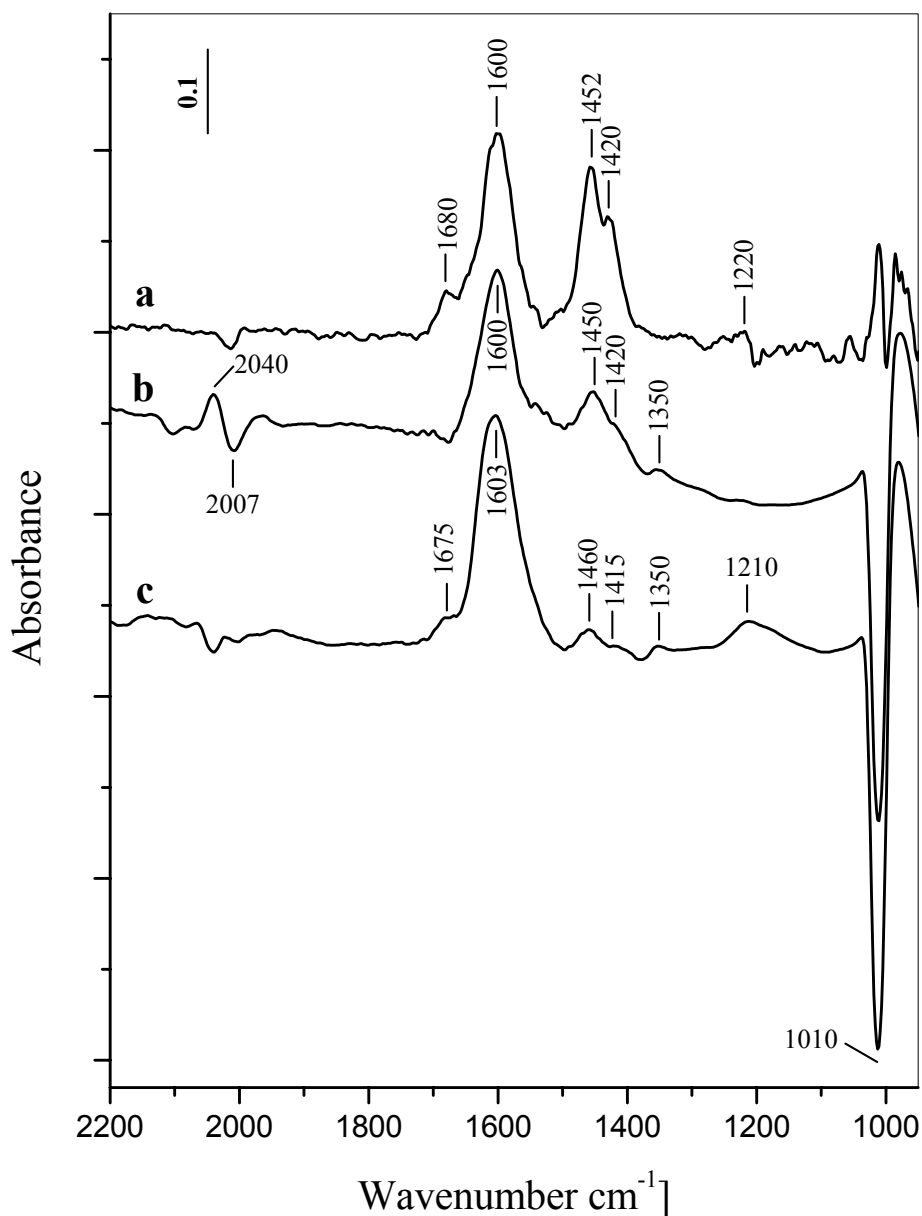
After the formation of NO<sub>x</sub> species on the WZ support by room temperature adsorption of NO/O<sub>2</sub> followed by evacuation for 15 min (Fig. 23, spectrum a), methane (7.33 kPa) was added (Fig. 23, spectrum b). Then the closed



IR cell was heated in the 573 – 723 K temperature range. The spectrum taken at 573 K (Fig. 23, spectrum at 573 K) shows considerable decrease in the intensities of the nitrate bands and restoration of the perturbed  $W^{6+} = O$  groups (strong decrease in the intensity of the negative band at  $1012\text{ cm}^{-1}$ ). The positive band at  $1000\text{ cm}^{-1}$  corresponds to the restored  $W^{6+} = O$  groups, which differ from the originally present. The increase in the temperature to 723 K leads again to perturbation of the wolframyl species (the negative band at  $1012\text{ cm}^{-1}$  appears in the spectra from d to f with growing intensity). This can be explained by assuming that the tungsten(VI) ions, but not the  $NO_x$  species, are involved in the interaction with methane. The adsorbed  $NO_3^-$  species most probably block the active sites for methane oxidation and the oxidation process starts at 623 K, after the nitrates leave the surface. This temperature is by approximately 100 K higher than the temperature at which oxidation products of methane on the surface of the  $NO_x$ -free sample are detected (523 K, See Section 3.3.2.1, Fig. 20). The spectrum taken at room temperature (Fig. 23, spectrum c) contains bands, which can be assigned to bidentate ( $1602\text{ cm}^{-1}$ ) and monodentate carbonates ( $1450$  and  $1420\text{ cm}^{-1}$ ). The weak band at  $2040\text{ cm}^{-1}$  can be attributed to CO adsorbed on  $W^{4+}$  ions [80]. The negative band at  $2012\text{ cm}^{-1}$  is due to the overtone of the perturbed  $W^{6+} = O$  groups at  $1010\text{ cm}^{-1}$ . It should be pointed out that, as in the case of the “Blank  $NO_x$ ” experiment, the gas-phase spectrum does not contain  $NO_x$  species.



**Figure 23.** FT-IR spectra of the WZ support taken after adsorption of NO/O<sub>2</sub> mixture (1.33 kPa:2.66 kPa, NO:O<sub>2</sub> = 1:2) at RT followed by evacuation for 15 min (a) and addition of 7.33 kPa of CH<sub>4</sub> (b), after heating of the closed IR cell for 20 min and then cooling to RT (c), subsequently evacuation of the gas phase at RT (d). The spectrum of the activated sample is used as a background reference.



**Figure 24.** FT-IR spectra of the WZ support taken from the “Blank CH<sub>4</sub>” (a), the interaction of the preadsorbed NO<sub>x</sub> with CH<sub>4</sub> (b) and the “Blank NO<sub>x</sub>” (c) experiments after the final evacuation at room temperature. The spectrum of the activated sample is used as a background reference.

Figure 24 compares the spectra of the WZ sample obtained in the “Blank CH<sub>4</sub>” (spectrum a), “CH<sub>4</sub>-NO<sub>x</sub>” (spectrum b) and “Blank NO<sub>x</sub>” (spectrum c) experiments after the final evacuation at room temperature (see Fig. 20, spectrum after evacuation at RT; Fig. 23, spectrum d; Fig. 18, spectrum d).

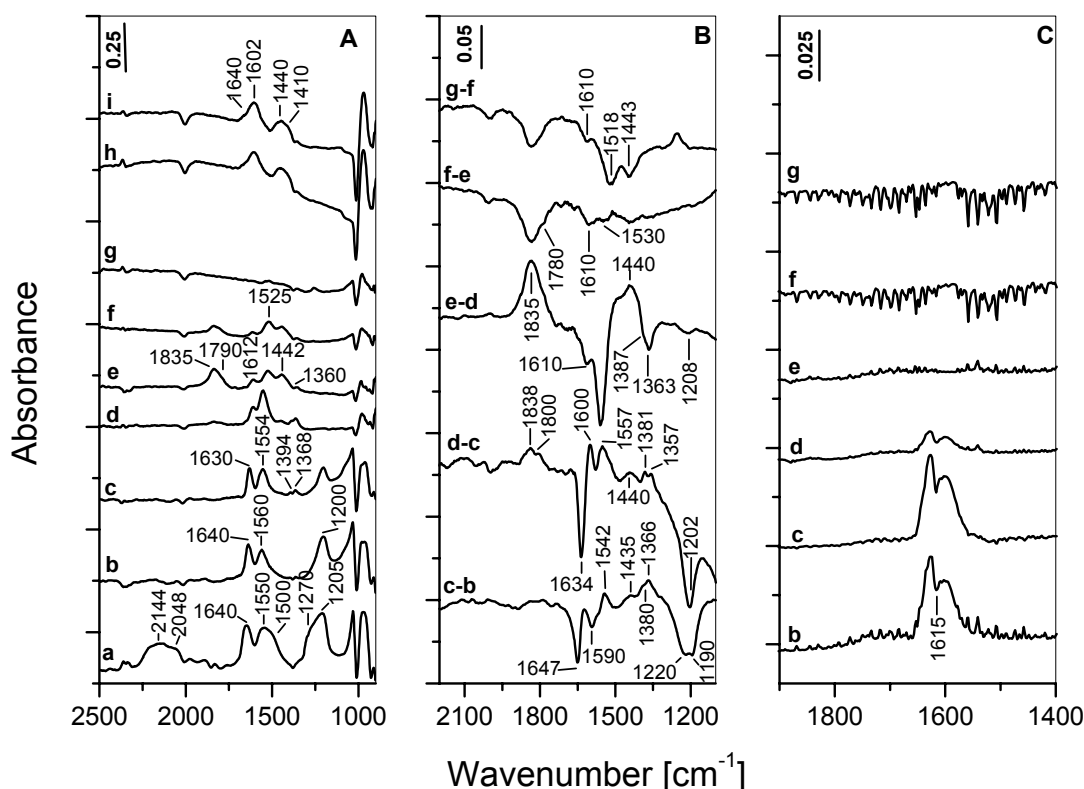
Intensities of the carbonate bands in spectrum b are lower than those in spectrum a. Moreover, by comparing spectra a and b it can be seen that the ratio of the intensities of the bands at  $1600\text{ cm}^{-1}$  versus those at  $1450$  and  $1420\text{ cm}^{-1}$  differs. The intensity of the band at  $1600\text{ cm}^{-1}$  in spectrum b relative to those at  $1450$  and  $1420\text{ cm}^{-1}$  is much higher. This difference can be explained by taking into account the spectrum c obtained in the “Blank  $\text{NO}_x$ ” experiment. In absence of interaction between the methane and the surface nitrates relatively strong nitrate band at  $1603\text{ cm}^{-1}$  is present in spectrum c. It can be assumed that the nitrate and bidentate carbonate bands in the spectrum b obtained in the “ $\text{CH}_4\text{-NO}_x$ ” experiment are superimposed, which leads to enhancement of the intensity of the band at  $1601\text{ cm}^{-1}$ . In addition, the spectrum from the “Blank  $\text{CH}_4$ ” experiment taken at room temperature in the presence of the gas phase (Section 3.3.2.1, Fig. 20, spectrum d) contains sharp band at  $2362\text{ cm}^{-1}$  corresponding to adsorbed  $\text{CO}_2$ . Under the same conditions, in the “ $\text{CH}_4\text{-NO}_x$ ” experiment, no adsorbed  $\text{CO}_2$  is detected (Fig. 23, spectrum c). These data clearly illustrate that the preadsorbed  $\text{NO}_x$  species on the surface of the tungstated zirconia suppress the oxidation of methane.

### 3.3.2.2. On The Pd/WZ Catalyst

Stable  $\text{NO}_x$  species were created on the Pd/WZ sample as described in the previous section and then  $7.33\text{ kPa}$  of  $\text{CH}_4$  was added (Fig. 25, spectrum a).

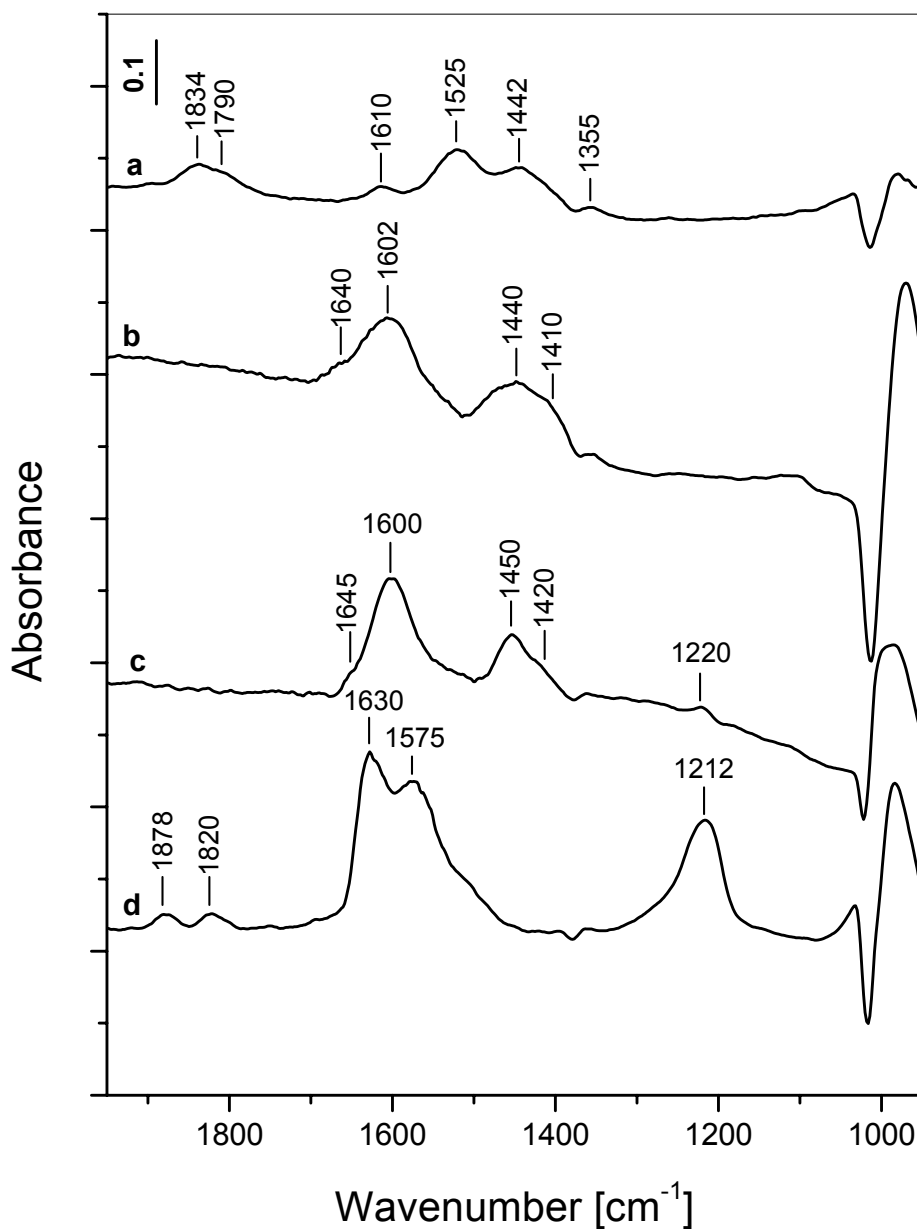
The treatment at  $473\text{ K}$  (Fig. 25(A), spectrum b) causes disappearance of the  $\text{NO}^+$  species (broad absorption between  $2250$  and  $2000\text{ cm}^{-1}$ ), Pd(II) nitrosyls ( $1876$  and  $1824\text{ cm}^{-1}$ ) and decomposition of the monodentate nitrates (unresolved bands at about  $1500$  and  $1270\text{ cm}^{-1}$ ). In the gas phase formation of  $\text{NO}_2$  is detected (Fig. 25(C), spectrum b). Further increase in the temperature to  $523\text{ K}$  (Fig. 25(A), spectrum c and Fig. 25(B), spectrum b-c) results in loss of the bridged ( $1647$  and  $1190\text{ cm}^{-1}$ ) and bidentate ( $1590$  and  $1220\text{ cm}^{-1}$ ) nitrates leading to additional increase in the amount of gaseous  $\text{NO}_2$  (Fig. 25(C), spectrum c). The weak positive bands at  $1542$ ,  $1435$ ,  $1380$  (shoulder) and  $1366\text{ cm}^{-1}$  in the subtraction spectrum b-c indicate formation of new species. At  $573\text{ K}$  (Fig. 25(A), spectrum d) all of the surface nitrates have decomposed, which is evident by the absence of the band at  $1200\text{ cm}^{-1}$  corresponding to the  $\nu_{\text{as}}(\text{NO}_2)$  modes (see also the subtraction spectrum d-c in Fig. 25(B)). However, no further increase in the

amount of the gaseous  $\text{NO}_2$  is detected (Fig. 25(C), spectrum d). In contrary, there is a strong decrease in the intensity of its IR band. This experimental fact leads to the conclusion that at 573 K  $\text{NO}_2$  does not leave the surface. It is consumed for the formation of the new species, whose spectral features are clearly observed as positive bands at 1557, 1440, 1381 and 1357  $\text{cm}^{-1}$  in the subtraction spectrum d-c (Fig. 25(B)).



**Figure 25.** (A) FT-IR spectra of the Pd/WZ catalyst taken after adsorption of  $\text{NO}/\text{O}_2$  mixture (1.33 kPa:2.66 kPa,  $\text{NO}:\text{O}_2 = 1:2$ ) at RT followed by evacuation for 15 min and addition of 7.33 kPa of  $\text{CH}_4$  (a), after heating of the closed IR cell for 15 min at 473 K (b), 523 K (c), 573 K (d), 623 K (e), 673 K (f), 723 K (g) and then cooling to RT (h), subsequently evacuation of the gas phase at RT (i). The spectrum of the activated sample is used as a background reference. (B) FT-IR subtraction spectra of the Pd/WZ catalyst obtained from the spectra shown in panel A. (C) Gas phase spectrum of the corresponding spectrum shown in panel A.

These bands cannot be assigned to inorganic  $\text{NO}_2^-$  (nitro) species produced by transformation of the adsorbed nitrates because in the “Blank  $\text{NO}_x$ ” experiment with the Pd/WZ catalyst no such bands are detected (Section 3.3.1.2, Fig. 19). Based on literature data [53,56,57,80], the bands at 1557, 1440, 1381 and 1357  $\text{cm}^{-1}$  are attributed to the  $\nu_{\text{as}}(\text{NO}_2)$ ,  $\delta_{\text{as}}(\text{CH}_3)$ ,  $\nu_{\text{s}}(\text{NO}_2)$  and  $\delta_{\text{s}}(\text{CH}_3)$  of adsorbed  $\text{CH}_3\text{NO}_2$ , respectively. The positive band at 1600  $\text{cm}^{-1}$  is assigned to adsorbed  $\text{NO}_2$  (see section high-temperature adsorption of NO). The weak band at 1838  $\text{cm}^{-1}$  with shoulder at 1800  $\text{cm}^{-1}$  present in the subtraction spectrum d-c increase significantly in intensity at 623 K (Fig. 25(A), spectrum e and 25(B), spectrum e-d). This is accompanied by decrease in the amount of adsorbed  $\text{NO}_2$  (negative band at 1610 and 1208  $\text{cm}^{-1}$ ) and disappearance of the adsorbed nitromethane (negative bands at 1557, 1387 and 1363  $\text{cm}^{-1}$ ). Formation of new species (which will be identified below) exhibiting absorption bands at 1525, 1442 and 1360  $\text{cm}^{-1}$  is detected (Fig. 25(A), spectrum e). The bands at 1835 and 1790  $\text{cm}^{-1}$  (Fig. 25(A), spectrum e and Fig. 25(B), spectrum e-d) correspond to NO adsorbed on two different Pd(I) sites. Obviously, the adsorbed NO arises as a decomposition product of the nitromethane. The heating at 673 K (Fig. 25(A), spectrum f and Fig. 25(B), spectrum f-e) affects considerably the intensities of the  $\text{Pd}^+-\text{NO}$  nitrosyl bands. This decrease could be associated with interaction of the transformation product(s) with the adsorbed NO or its oxidation to  $\text{NO}_2$ . However, the latter process is not likely to occur because there is decrease in the intensity of the band at 1610  $\text{cm}^{-1}$  (Fig. 25(A), spectrum f, Fig. 25(B), spectrum f-e). Raising the temperature to 723 K (Fig. 25(A), spectrum g) results in complete disappearance of all of the adsorption bands. The spectrum taken after cooling to room temperature displays bands, which fall in the carbonate-carboxylate region (Fig. 25, spectra h and i). Fig. 26 compares the results of the “ $\text{NO}_x\text{-CH}_4$ ”, “Blank  $\text{CH}_4$ ” and “Blank  $\text{NO}_x$ ” experiments. The spectra obtained after the interaction of the  $\text{CH}_4$  with the  $\text{NO}_x$ -precovered and  $\text{NO}_x$ -free Pd/WZ catalyst are similar, which shows that the main products in both cases are adsorbed carbonate species.

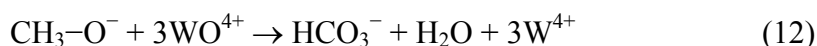
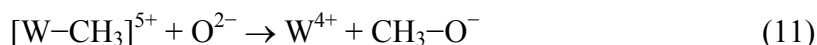


**Figure 26.** FT-IR spectra of the Pd/WZ catalyst taken from the interaction of the preadsorbed  $\text{NO}_x$  with  $\text{CH}_4$  at 673 K (a) and after evacuation at room temperature (b), the “Blank  $\text{CH}_4$ ” (c), and the “Blank  $\text{NO}_x$ ” (d) experiments after the final evacuation at room temperature. The spectrum of the activated sample is used as a background reference.

### 3. 4. Summary of the Results on the Reactivity of the Adsorbed NO<sub>x</sub> Species toward Methane

The experimental results show that the CH<sub>4</sub> interacts in a different way with the NO<sub>x</sub>-precovered tungstated zirconia and Pd/WZ catalyst although both materials are able to activate the hydrocarbon at the same temperature in absence of adsorbed NO<sub>x</sub> species. In the case of the WZ sample, the surface nitrates suppress the oxidation of methane, whereas the NO<sub>x</sub>-precovered Pd/WZ sample catalyzes the formation of nitromethane.

Studies with oxide systems [82,83] have shown that methane is adsorbed dissociatively over strong Lewis acid-base pairs with generation of metal – alkyl and methoxy species. The following reaction steps can be proposed for the oxidation of the methane on the NO<sub>x</sub>-free WZ sample:



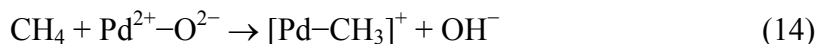
Scheme 1

It is assumed that steps from (10) to (12) are fast and therefore the methoxy species cannot be detected. This reaction scheme explains the negative effect of the preadsorbed NO<sub>x</sub> species on the activity of tungstated zirconia in the oxidation of methane in absence of molecular oxygen. The nitrates formed by room-temperature adsorption of NO/O<sub>2</sub> do not interact with methane and block the wolframyl groups considered as active sites for the hydrocarbon activation.

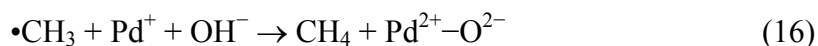
In the case of the Pd/WZ catalyst, there are two kinds of sites that are candidates for methane activation: the Pd(II) and W(VI) species. Reaction scheme analogous to Scheme 1, in which Pd(II) ions are involved, could operate as well with a change in the oxidation states of palladium from +2 to zero. However, the introduction of palladium to the tungstated zirconia did not increase the conversion of methane in the “Blank CH<sub>4</sub>” experiment. In contrary, the surface concentrations of the HCO<sub>3</sub><sup>-</sup> and CO<sub>3</sub><sup>2-</sup> produced on the Pd/WZ catalyst are lower than those on the tungstated zirconia (see Fig. 22).



Valyon et al. [83] proposed that if the  $\text{CH}_3^-$  groups cannot be stabilized by the oxide,  $\bullet\text{CH}_3$  radicals can be produced. In the case of the Pd/WZ catalyst the following reactions can be assumed:



The  $\bullet\text{CH}_3$  species following reaction (16) can convert back to methane:

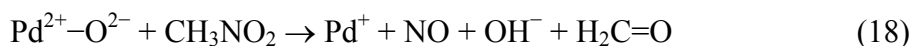


This process leads to decrease in the amount of the activated methane and can explain the lower conversion of the hydrocarbon on the Pd/WZ catalyst observed in absence of molecular oxygen compared to that on the WZ sample.

The formation of nitromethane on the  $\text{NO}_x$ -precovered Pd/WZ catalyst starts at 523 K. At this temperature the hydrocarbon is already activated on the  $\text{NO}_x$ -free catalyst: hydrogencarbonates and carbonates are detected indicating that the oxidation of the methane takes place in absence of molecular oxygen. It can be proposed that the  $\bullet\text{CH}_3$  radicals, which are produced according to reaction (15) are captured by the  $\text{NO}_2$  realized during the decomposition of the nitrate species (see Fig. 19, page 42):



The IR data obtained during the interaction of  $\text{CH}_4$  with the  $\text{NO}_x$ -precovered Pd/WZ catalyst show that at 623 K nitromethane transforms in the compound(s) characterized by the absorption bands at 1525, 1442 and  $1360\text{ cm}^{-1}$  and NO adsorbed on Pd(I) sites (Fig. 25(A), spectrum e). The weak band at  $1612\text{ cm}^{-1}$  belongs to adsorbed  $\text{NO}_2$ , which resists even the evacuation at 623 K as shown in Section 3.2.3. It can be proposed that the nitromethane undergoes reductive transformation according to the following reaction:

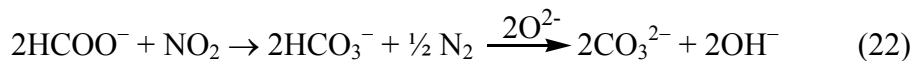
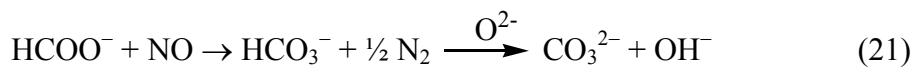


The formaldehyde is unstable on oxide surfaces [84,85] and can be oxidized fast by the Pd(II) to formic acid:



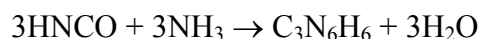
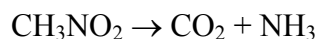
The bands at 1525 and  $1360\text{ cm}^{-1}$  (Fig. 25(A), spectra e and d) are assigned to the  $\nu_{\text{as}}(\text{CO}_2)$  and  $\nu_{\text{s}}(\text{CO}_2)$  stretching modes of bidentate formate ion [67,68,78], whereas the band at  $1442\text{ cm}^{-1}$  most probably is due to monodentate carbonate [67]. The latter species can be formed either by decomposition of the formate

(reaction 20) or by oxidation of the  $\text{HCOO}^-$  with the adsorbed NO and  $\text{NO}_2$  (reactions 21):



Oxidation of the formaldehyde by NO or  $\text{NO}_2$  to formic acid and/or carbonates is not excluded. This assumption (reactions 21) is supported by the fact that the bands due to the formate species decrease in intensity at 673 K and disappear together with the adsorbed NO and  $\text{NO}_2$  at 723 K. The carbonates at  $1442 \text{ cm}^{-1}$  desorb also at 723 K. After cooling to room temperature bidentate ( $1602 \text{ cm}^{-1}$ ) and monodentate carbonates (broad band with maximum at  $1440 \text{ cm}^{-1}$ ) are detected. Some amount of hydrogencarbonates is observed as well (band at  $1640 \text{ cm}^{-1}$ ). It should be pointed out that Beloshapkin et al. [56] reported also formation of adsorbed NO during the thermal transformation of nitromethane on Co-ZSM-5 at 553 K.

Sun et al. [52] first observed, by means of DRIFT, the formation of  $\text{CH}_3\text{NO}_2$  on the Co-ZSM-5 and proposed this compound as an intermediate in the SCR of NO with  $\text{CH}_4$  in presence of oxygen. Since then a vast amount of studies [54,55,85], mainly on zeolitic catalysts, is devoted to the investigation of the routes of nitromethane transformations to yield the products of the  $\text{CH}_4$ -SCR:  $\text{N}_2$ ,  $\text{CO}_2$  and  $\text{H}_2\text{O}$ . In general, the following overall scheme for Co-ZSM-5 as catalyst is widely accepted, which involves very fast steps of nitromethane transformation [54,55,86-88]:



The intermediate formation of ammonia, which is an efficient reducing agent of NO, can lead to the products of the SCR. Watson and Ozkan [51] observed formation of  $\text{NH}_3$  during the interaction of  $\text{NO} + \text{O}_2 + \text{CH}_4$  mixture on Pd/TiO<sub>2</sub> catalyst.

The final transformation product, the cyclic compound  $\text{C}_3\text{N}_6\text{H}_6$  (melamine), is detected during the decomposition of nitromethane on Co-ZSM-5 at elevated temperatures giving rise to a sharp tailing band at  $1662 - 1665 \text{ cm}^{-1}$

[56, 88]. No such a band is present in the spectra taken above 573 K in the case of the Pd/WZ catalyst. The melamine can be removed at 673 K by heating in oxygen [56].

The difference in the reactivity of the NO<sub>x</sub>-precovered tungstated zirconia and Pd-containing tungstated zirconia toward methane lies in the ability of the Pd/WZ catalyst to stabilize adsorbed NO<sub>2</sub> to relatively high temperatures (573 – 623 K). According to the experimental results the highest concentration of NO<sub>2</sub> adsorbed on the Pd/WZ catalyst is reached at 573 K, after the complete decomposition of the surface nitrates. In the case of the tungstated zirconia, no adsorbed NO<sub>2</sub> is detected at temperatures higher than the room temperature and in absence of NO/O<sub>2</sub> mixture. According to the results of the “Blank NO<sub>x</sub>” and “CH<sub>4</sub>-NO<sub>x</sub>” experiments with the WZ sample, the spectrum of the gas phase taken after the heating at 723 K does not contain gaseous NO<sub>x</sub> species. This indicates that the nitrates formed on the tungstated zirconia follow decomposition route different from that on the Pd/WZ catalyst. Most probably the gas phase in the former case contains both NO and NO<sub>2</sub> in low concentrations, which cannot be measured under the conditions of the existing path length of the IR cell. However, heating the NO<sub>x</sub>-precovered Pd/WZ catalyst in the 523 – 723 K temperature range causes release of significant amount of NO<sub>2</sub> in the gas phase, which readsorbs at room temperature producing surface nitrates (Section 3.3.1.2, Fig. 19, spectra a and evacuation at RT). It can be concluded that the role of the nitrate species adsorbed on the Pd/WZ catalyst is to provide high surface concentration of NO<sub>2</sub> at high temperatures, which can interact with the hydrocarbon producing nitromethane.

## 4. CONCLUSIONS

1. The structures of the tungstated zirconia and palladium(II) supported on tungstated zirconia have been studied by means of XRD and FT-IR spectroscopy. Tungstated zirconia was prepared by coprecipitation of solutions of  $\text{ZrOCl}_2 \cdot \text{H}_2\text{O}$  and ammonium metatungstate using polyvinyl alcohol as a template. According to the XRD the sharp peak at low angle ( $2\theta = 1.8^\circ$ ) shows formation of a mesoporous phase in the sample. The presence of  $\text{WO}_x$  groups and the mesoporosity ensure 100% tetragonal phase and small crystallites ( $\sim 5$  nm). The sample has high surface area compared to samples synthesized by conventional impregnation techniques. The introduction of palladium(II) using solution of Pd(II) nitrate affect considerably the amount of the mesoporous phase. The FT-IR spectra of the activated tungstated zirconia and Pd/tungstated zirconia reveal presence of  $\text{W}^{6+}=\text{O}$  groups.

2. The adsorption of NO on tungstated zirconia at room temperature allows detection of coordinatively unsaturated Zr(IV) ions. The wolframyl groups oxidize the adsorbed NO to  $\text{N}_2\text{O}_3$  and  $\text{NO}_2^-$  species. The spectrum of NO on Pd/tungstated zirconia reveals the presence of two types of Pd(II) sites. No exposed Zr(IV) ions are observed. The surface  $\text{NO}_x$  species ( $\text{N}_2\text{O}_3$ , nitro and nitrito ions) as in the case of tungstated zirconia, are produced by oxidation of NO with the wolframyl species and the palladium(II) is not involved. However, the latter can oxidize the adsorbed NO to  $\text{NO}_2$  at 623 K.

3. Upon coadsorption of NO and  $\text{O}_2$  at room temperature on the samples studied, various kinds of surface nitrates are observed differing in the modes of their coordination. The thermal stability of the nitrate species formed on both materials is comparable. However, the concentration of the surface nitrates is lower for the Pd-containing sample, which indicates that the  $\text{NO}_3^-$  species formed on the latter are coordinated to the support.

4. The  $\text{NO}_x$ -free tungstated zirconia and Pd/tungstated zirconia are able to activate the methane already at 523 K in absence of molecular oxygen. However, judging from the intensities of the oxidation products (hydrogencarbonates and carbonates) the conversion of the hydrocarbon is lower for the Pd-containing

sample. This difference is explained by assuming destabilization of the metal-alkyl complex produced by dissociative adsorption of the methane in the presence of Pd(II) and formation of CH<sub>3</sub> radicals, which can recombine with surface protons back to methane.

5. In absence of molecular oxygen, the preadsorbed surface nitrates have negative effect on the activity of tungstated zirconia in the oxidation of methane. They do not interact with the hydrocarbon and block the wolframyl groups considered as active sites for the hydrocarbon activation.

6. In the case of the Pd/tungstated zirconia, the CH<sub>3</sub> radicals produced during the direct activation of the methane by the catalyst are captured by the NO<sub>2</sub> realized by the decomposition of the nitrate species, thus producing nitromethane. The highest surface concentration of nitromethane is detected at 573 K, after the complete decomposition of the NO<sub>3</sub><sup>-</sup> species. Increasing the temperature above 573 K causes transformation of the nitromethane to NO adsorbed on Pd(I) sites and partially oxidized hydrocarbon, most probably formaldehyde. The latter undergoes fast oxidation to formate species, which interact with the adsorbed NO giving the products of the CH<sub>4</sub>-SCR of NO: N<sub>2</sub>, CO<sub>2</sub> and H<sub>2</sub>O.

7. The role of WO<sub>3</sub> as modifier of the zirconia is to create high surface acidity of the support needed for the activation of methane. The addition of palladium(II) insures sufficient amounts of CH<sub>3</sub> radicals and adsorbed NO<sub>2</sub> resulting in the formation of nitromethane, the intermediate of the SCR of NO with methane in the presence of Pd/tungstated zirconia.

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